

High-temperature heat pumps

and the bio-/pharma industry



High-Temperature
Heat Pump Symposium



Project 68
Industrial High-Temperature
Heat Pumps



IEA HPT Project 68

Industrial High-Temperature Heat Pumps



14 countries confirmed, 1 strong interest



June 2025 to May 2028



Task 1 – Technology developments (Lead: DTI)

- Keep track of current and future technologies
- Provide updated overview

New update
in October!



Task 2 – Sector collaborations (Lead: Uni-P)

- Highlight potential across sectors
- Identify common technology gaps
- Develop solutions to current barriers



Task 3 – Education materials (Lead: AIT)

- Industry (end-users, consultants, suppliers, management...), academia, governments

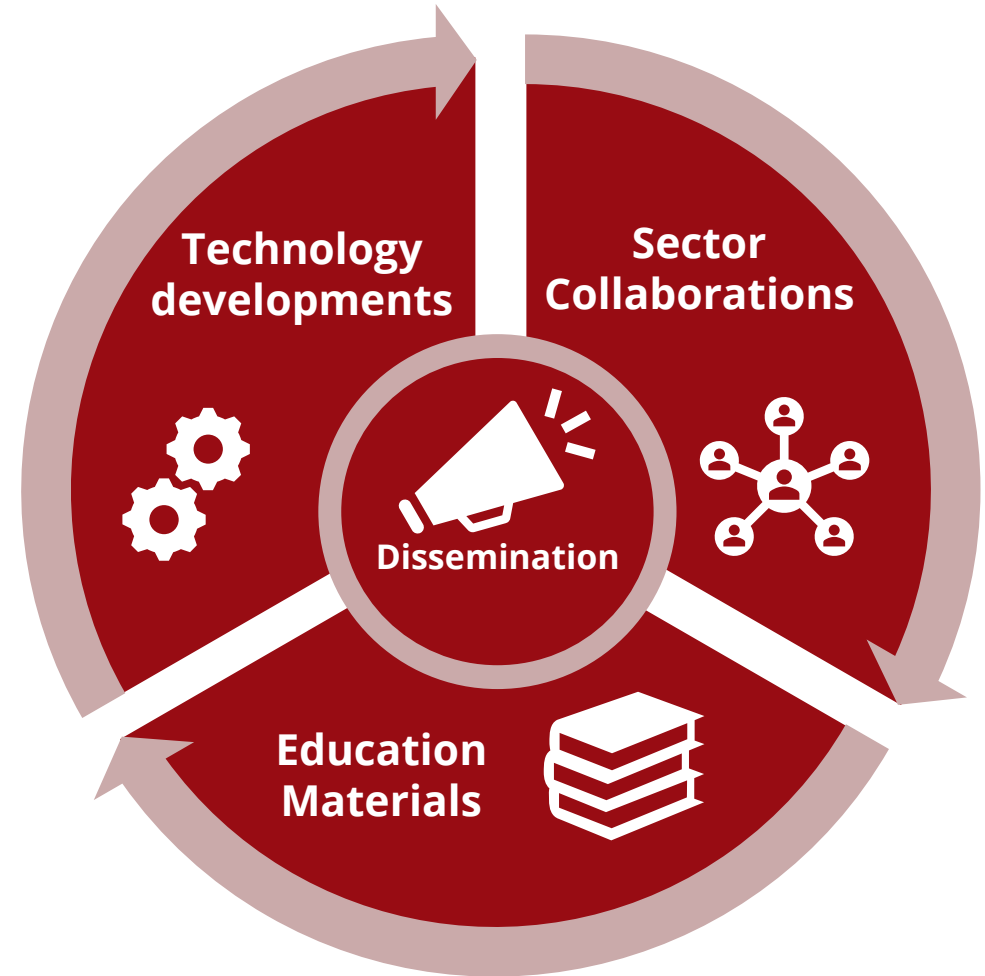


Project Management:

- Benjamin Zühlsdorf, bez@dti.dk &
- Martin Pihl Andersen, mapa@dti.dk



DANISH
TECHNOLOGICAL
INSTITUTE





HTHP Symposium



- Meeting place for HTHP Community
- 02/2028 – Copenhagen
- +120 presentations
- +35 exhibition stands
- +550 participants



DANISH
TECHNOLOGICAL
INSTITUTE



Sustainability Phorum Overview 2026

**CONNECT
COLLABORATE
ACCELERATE™**

BioPhorum: a co-ordinated program of industry change

BioPhorum is at the heart of pharmaceutical manufacturing, addressing industry issues and shaping best practice



Member-led



Safe and confidential



Cheaper, faster and better journeys



Consensus-driven

This allows for cost reduction, lower waste, improved productivity, better environmental performance across the value chain, better investment decisions and the cost of poor decisions avoided.

There are currently 12 Phorums providing a wealth of opportunities for companies to align their interests with similarly committed organizations.



300+

memberships

150+

global programs for change

5,000+

leaders and subject matter experts

170+

published papers, presentations and resources in the last 12 months

BioPhorum Sustainability



Steering Group

Drive industry-wide reductions in environmental impact (carbon, water, waste and nature) across supply chain, manufacturing and packaging.

Sustainable Supplies



Sustainable Manufacturing



Sustainable Packaging



Understand and Influence the operating environment - hear the voice of the customer and the supplier through in-person and virtual safes, hear from curated content of expert speakers and system stakeholders, translate sustainability strategy for a biomanufacturing audience, learn from peer case studies, engage with system stakeholders.



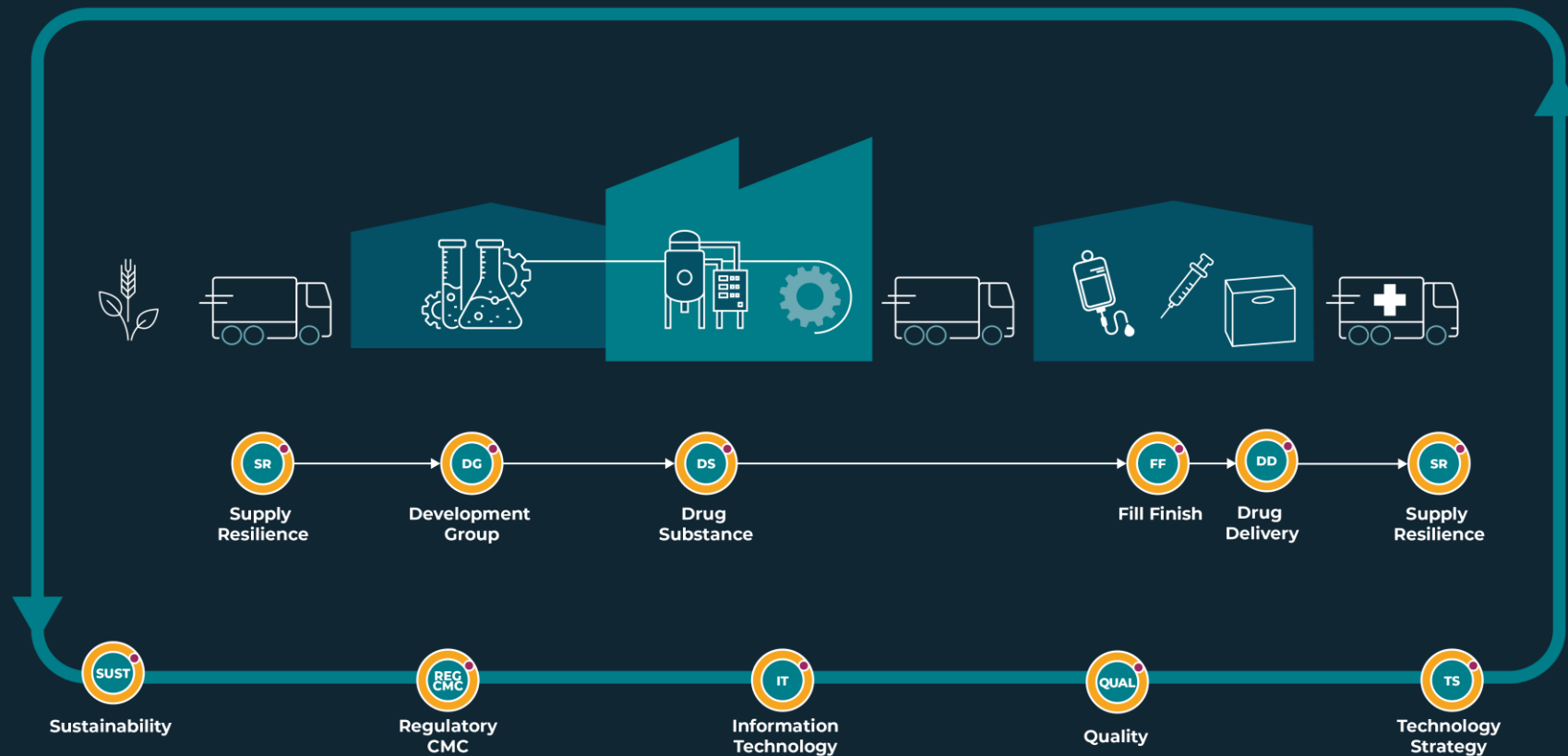
Build best practice – compare and define sustainability best practice, augment operational best practice with sustainability requirements, incubate operational changes that are not yet “commercially ready” by building the business case for change and removing quality and regulatory friction to accelerate adoption.



Assess – use the **BioPhorum Environmental Excellence Maturity Model** to understand performance across sites, peers and value chain partners and create roadmaps for change. Use **AskBioPhorum** to crowd source solutions to immediate challenges. Use tools like the **HVAC Optimization Tool** to build the case for change.

Embedding sustainability in operational excellence

BioPhorum acts as the translation layer – turning high-level sustainability strategies into practical, implementable programs for manufacturing, supply chain and product development teams. Through structured links between programs and Phorums – and active engagement with external bodies such as regulators, standards organizations, NGOs and industry initiatives – BioPhorum helps members connect sustainability initiatives that would otherwise remain isolated.





Energy



Water



Waste

Interest and relevance in HTHP technology

- Reducing reliance on natural gas is a key driver to reducing scope 1 and 2 emissions in biopharma manufacturing facilities - HTHP technology is a key enabler for this
- Our members see clear applications in energy intensive critical utilities within the biopharmaceutical industry such as Water For Injection (WFI) generation systems
- Being able to share case studies and discussing the opportunities is an important initial step into making real improvements

Webinar series continues

Today: 17th of September



HTHPs and the bio-/pharma
industry

Co-host:  **BioPhorum**

Next webinar: 2nd of December 2026



HTHPs for drying applications



3-4 times a year

Webinar
homepage



Info on next
webinars



**Including 40+ HTHP
operating cases!**



Today program

15:00	Welcome	
20 minutes	Decarbonization concepts for pharmaceutical production sites	
20 minutes	AHEAD – Pioneering CO ₂ -Free Steam Without Gas	
20 minutes	Steam generation for pharma industry using Stirling heat pumps	
20 minutes	Decarbonization concepts for pharmaceutical production sites	
End by 16:30	Concluding remarks	

Decarbonization concepts for pharmaceutical production sites

Anton Beck
Research engineer



DECARBONIZATION CONCEPTS FOR PHARMACEUTICAL PRODUCTION SITES

Project 68 Webinar series, Thursday, 17 September 2026:
HTHPs and the Bio-/Pharma Industry

Dipl.-Ing. Dr. Anton Beck

AIT – Center for Energy



DEKARBPHARM CONSORTIUM

Industry Association



Research



Industry Partners



Funding



FFG
Promoting Innovation.

 **Federal Ministry**
Republic of Austria
Climate Action, Environment,
Energy, Mobility,
Innovation and Technology

OVERVIEW



SCOPE OF THE
PROJECT



METHODOLOGY



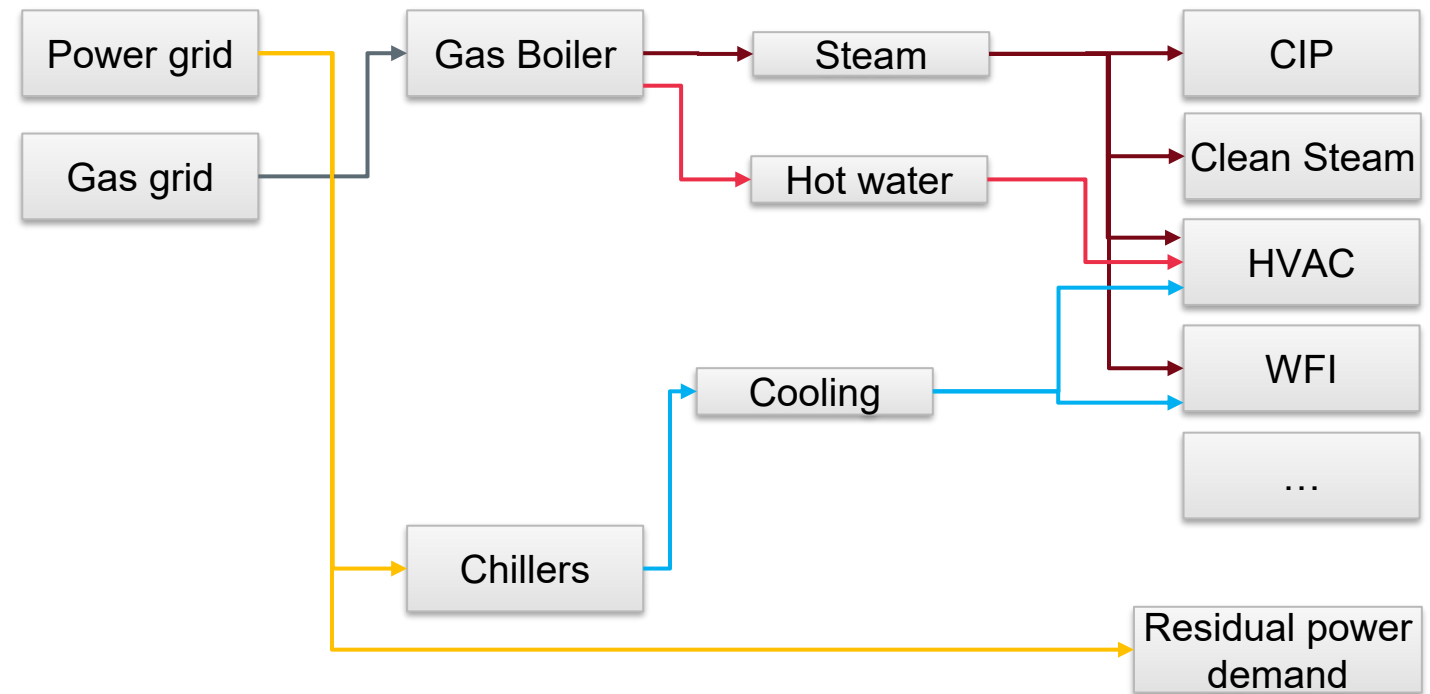
ENERGY EFFICIENCY &
HEAT PUMPS



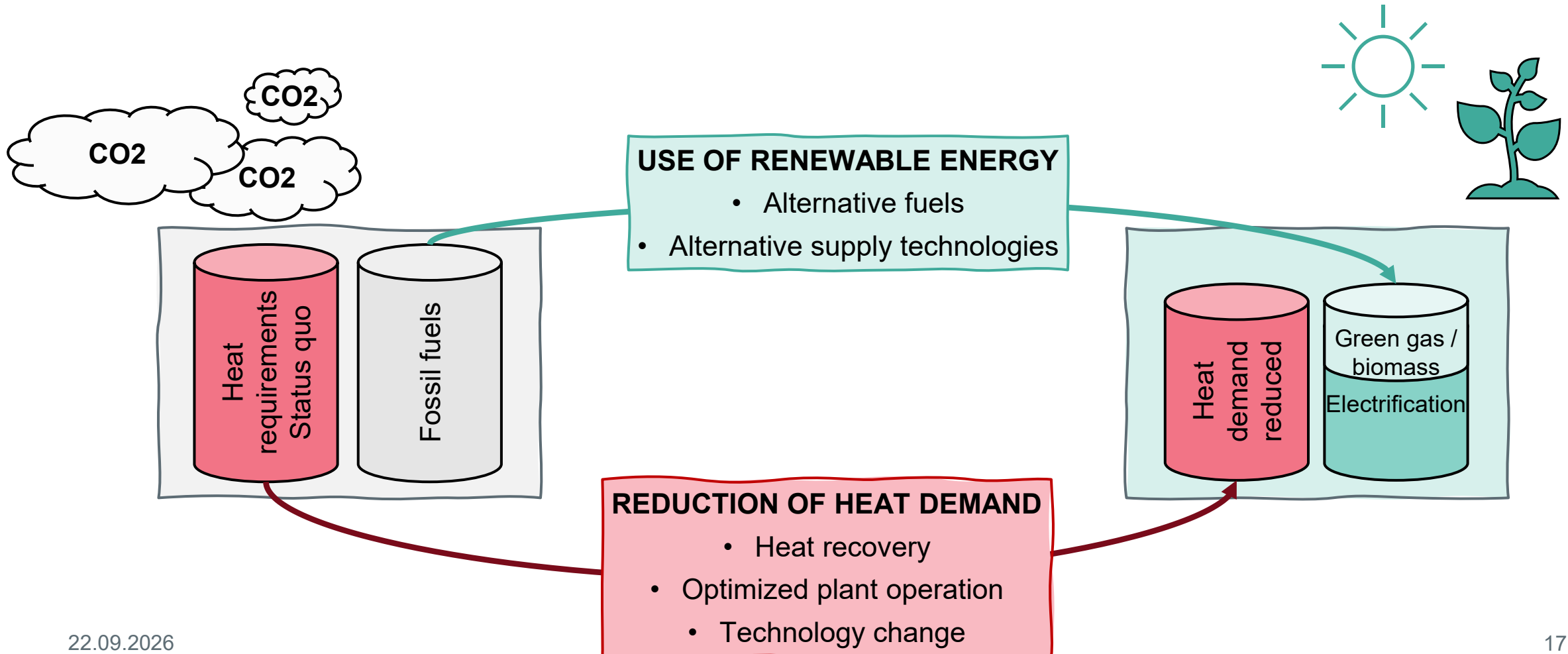
KEY FINDINGS

TYPICAL ENERGY SYSTEM

- Natural gas is main source for onsite CO₂ emissions
- Large cooling demand
→ excess heat potential
- Seasonal characteristics
 - Summer → cooling
 - Winter → heating



TRANSITION TOWARDS A RENEWABLE ENERGY SYSTEM



APPROACH



IDENTIFIED MEASURES

Tier 0: Status Quo

Tier 1: low impact, mostly utility system

- CIP: heat recovery from caustic rinse, heat supply with hot water instead of steam
- HVAC: fresh air preconditioning, internal heat recovery
- Heat recovery for heat pumps: Chillers, Compressors, Waste Water

Tier 2: moderate impact, revalidation likely

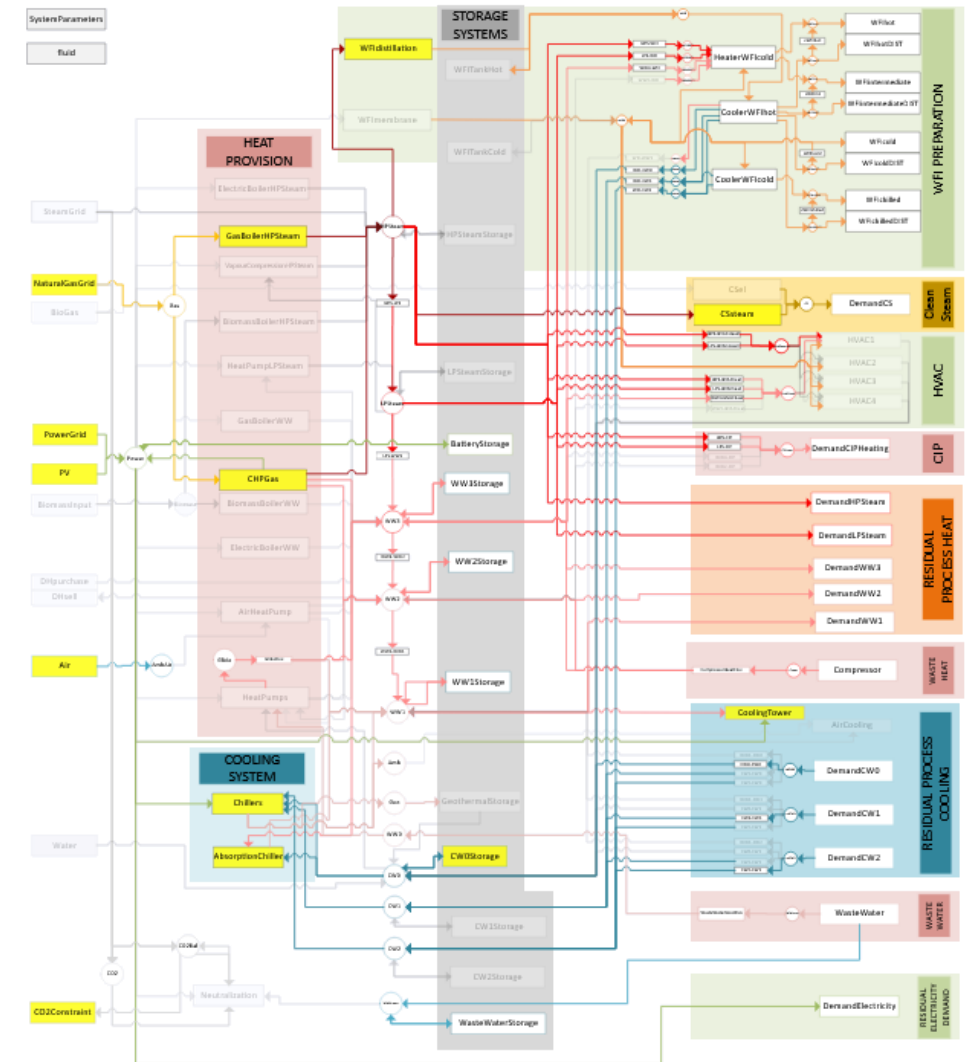
- HVAC: extend ranges for set points, adapt control strategy, reduce supply temperature for heating
- Clean steam: possibility to switch to direct electric steam generation

Tier 3: critical

- HVAC: adiabatic air humidification
- Membrane based WFI generation (now considered Tier 2)

SYSTEM MODEL

- Energy supply → energy conversion and storage → process demands (cooling, heating, clean media)
- Multiple **heat supply levels** (high pressure steam → sub ambient cooling)
- Important **process demands** explicitly modelled (HVAC, WFI-generation, CIP...)
- **Heat recovery** (off-steam, compressors, waste water)
- Investment decisions for **alternative systems** for heating, cooling and storage

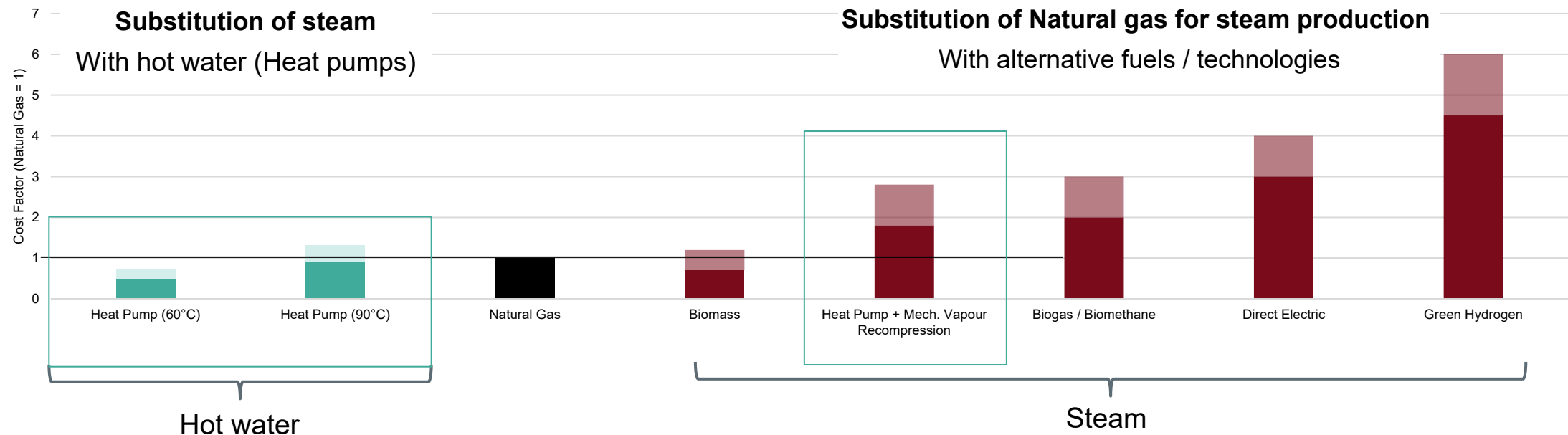


LOW-TEMPERATURE HEAT CAN BE ELECTRIFIED COST-EFFECTIVELY

Provision of process heat

Assumptions:

- Power to natural gas price ratio: 3–4
- 2nd law efficiency (heat pumps): 50–55 %
- Biogas to natural gas price ratio: 2–3
- biomass to natural gas price ratio : 0.7–1.2

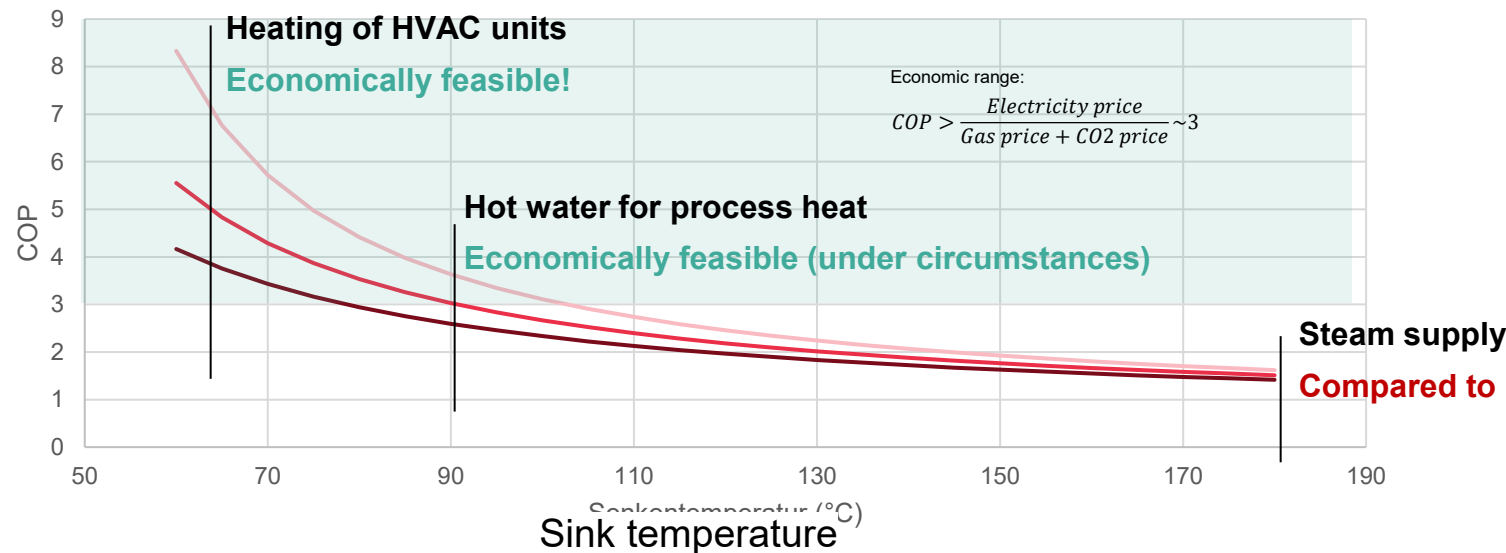


**Substitution of fossil-based steam
with renewables is usually expensive!**

HEAT-PUMP ECONOMICS DEPEND STRONGLY ON SINK TEMPERATURE

Heat supply with heat pumps

- **Demands:** Supply heat at temperatures as low as possible
- **Excess heat sources:** Temperatures as high as possible



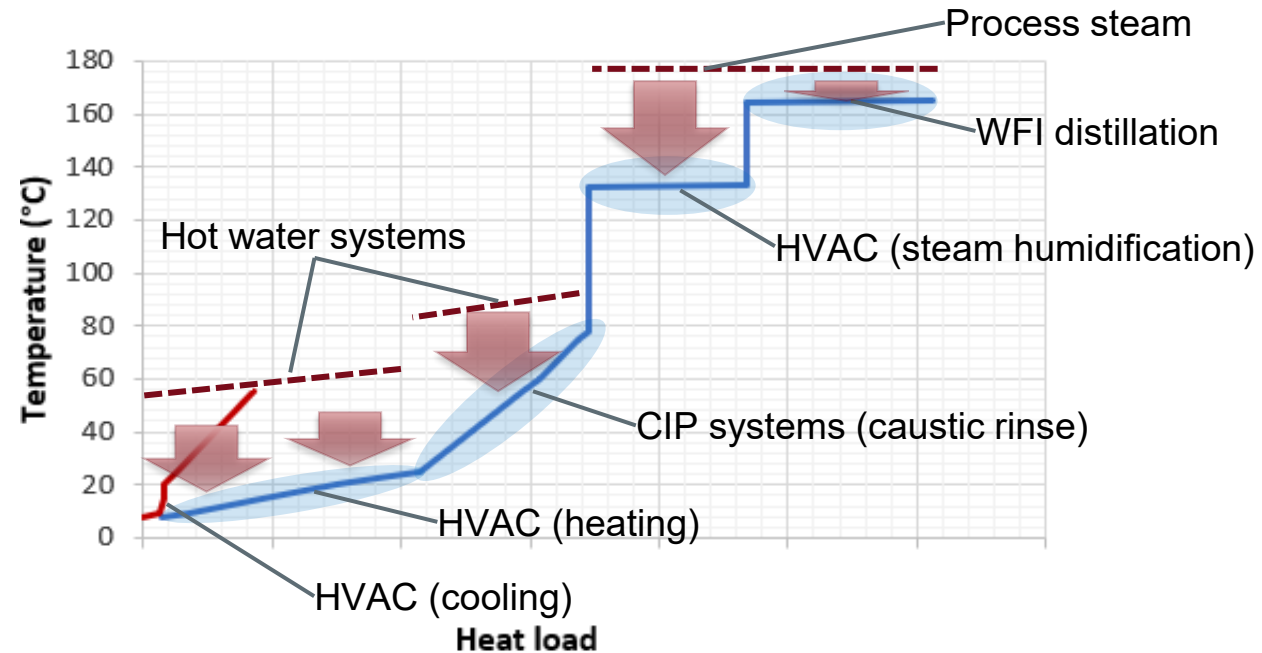
Source temperature 20 ° C – 2nd law efficiency: 0.50
 Source temperature 30 ° C – 2nd law efficiency: 0.50
 Source temperature 40 ° C – 2nd law efficiency: 0.50

ENERGY EFFICIENCY

ELECTRIFICATION – HEAT PUMPS

Substitution with hot water supply

- CIP systems (80 °C),
- HVAC (50-60 °C),
- Preheating of drying processes
- WFI sanitization (with cold WFI production),
- Heating of WFI loops (80 °C)
- Thawing processes,
- ...

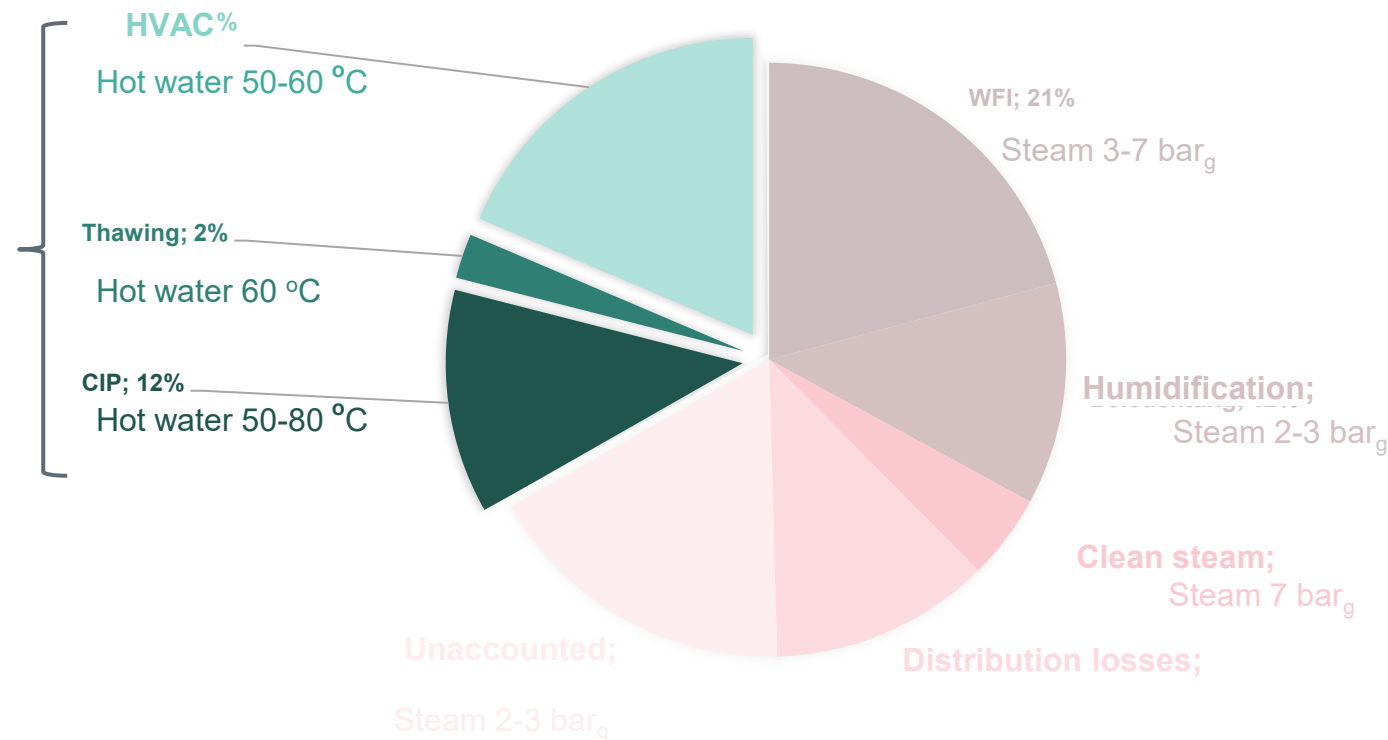


ABOUT ONE-THIRD OF HEAT DEMAND CAN BE SUPPLIED BELOW 80°C

Industry example – Potential for hot water

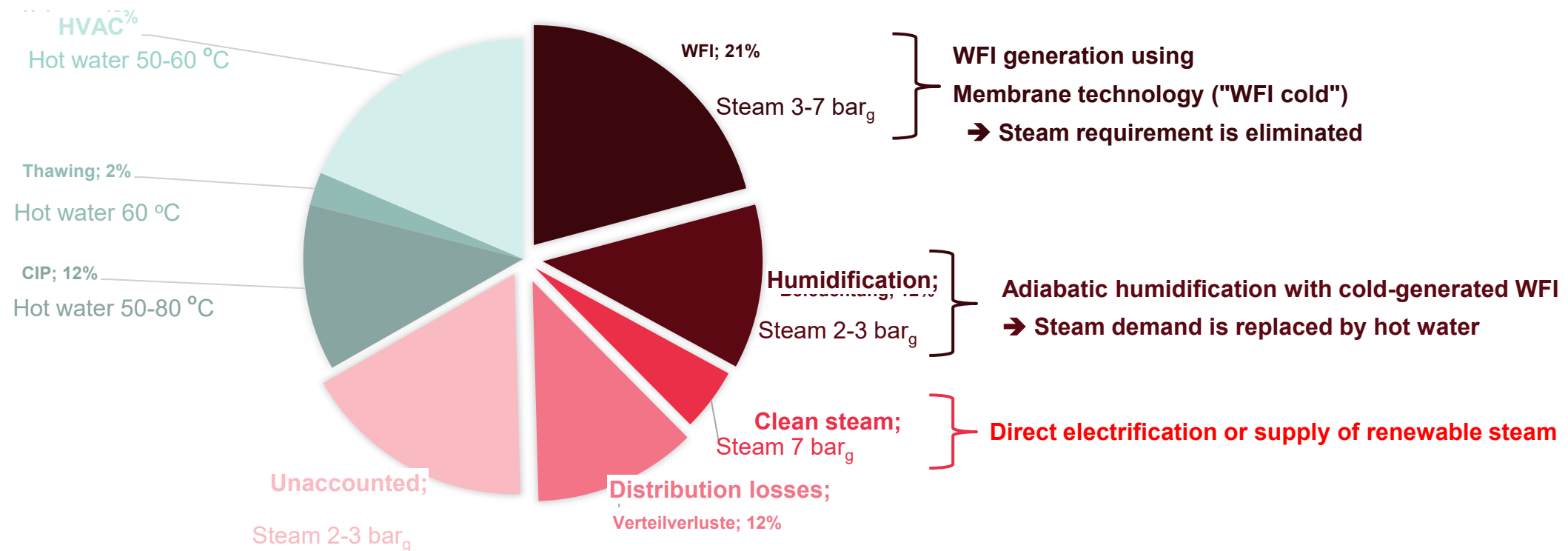
Potential savings through
heat pump use!

About **33% of heat
demand and of CO2
emissions**

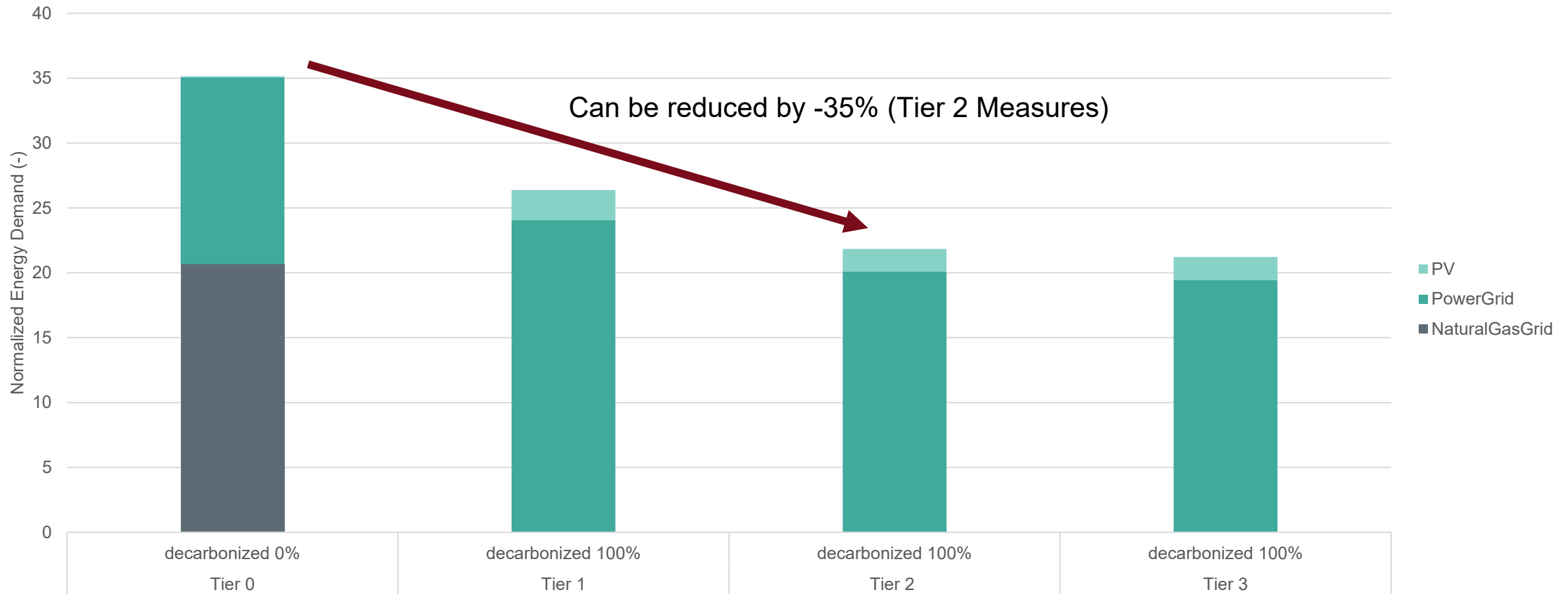


OVERVIEW OF HEAT DEMAND

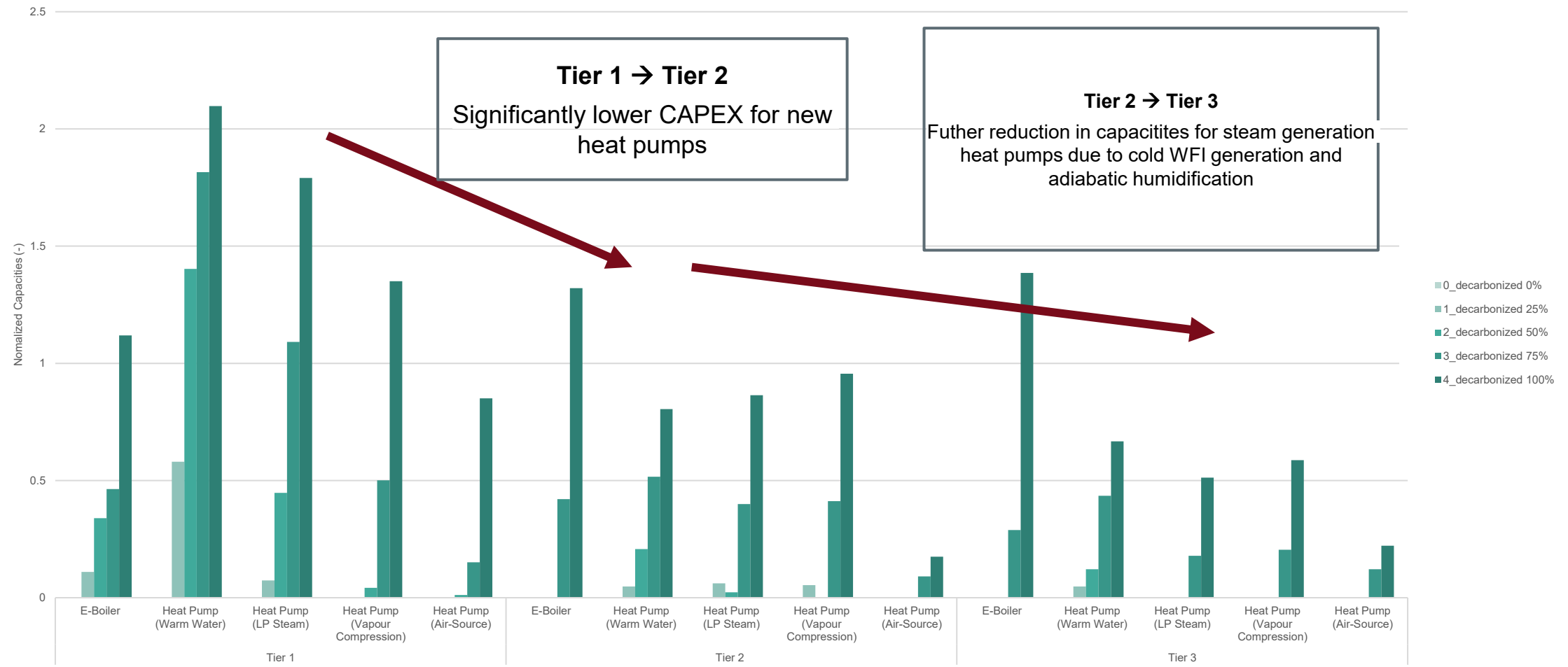
Industry example – Potential for technology change



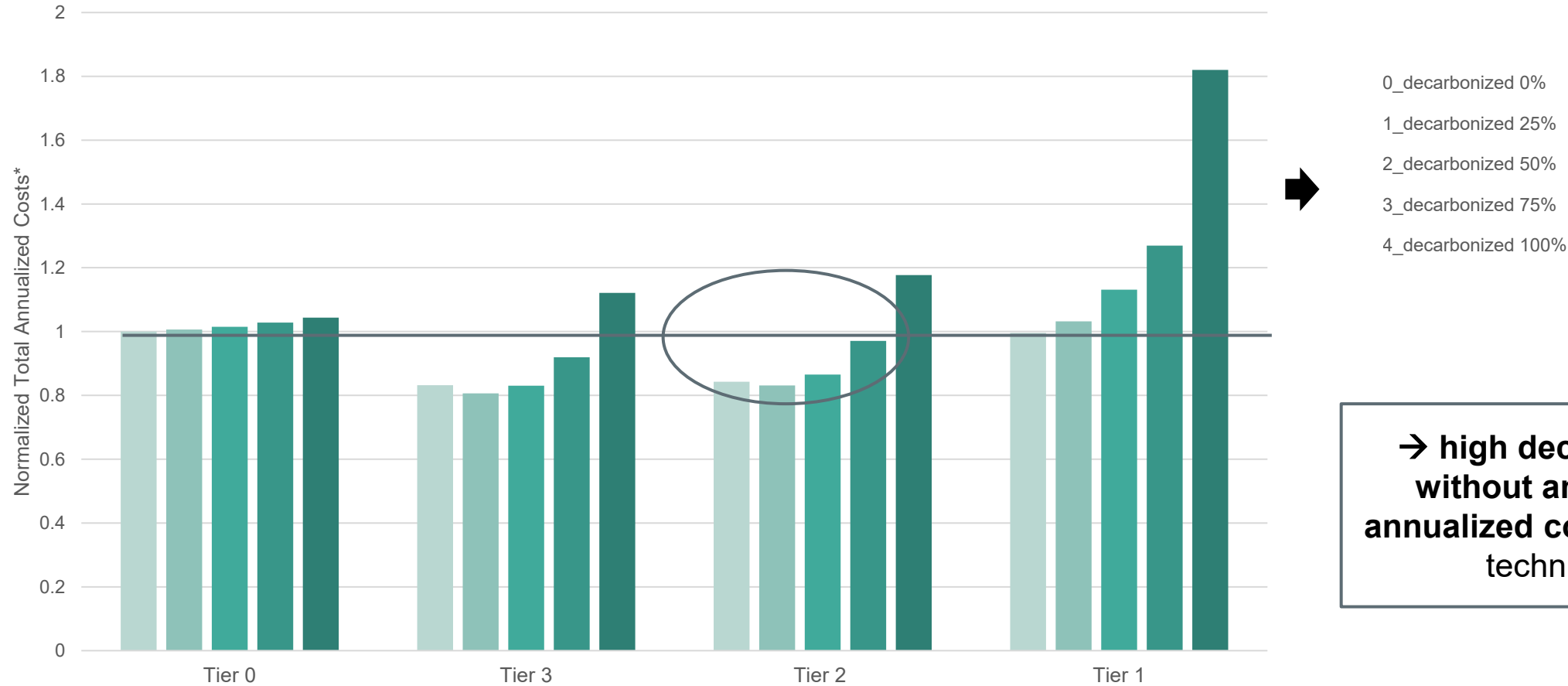
EFFICIENCY MEASURES REDUCE FINAL ENERGY DEMAND BY 35%



PROCESS CHANGES REDUCE REQUIRED HEAT-PUMP CAPACITIES



EFFICIENCY ENABLES HIGH DECARBONIZATION WITHOUT HIGHER ANNUAL COSTS



→ high decarbonization rates
without an increase in total
annualized costs for energy supply
technically possible

*10-year depreciation period

CONCLUSION



A large share of pharmaceutical heat demand can be supplied efficiently by heat pumps



Energy efficiency and heat recovery reduce both electricity demand and required heat pump capacity



Technology changes such as membrane-based WFI generation unlock deeper decarbonization at competitive annual costs

PHARMACEUTICAL SECTOR COLLABORATION



IEA Technology Collaboration Programme on
Heat Pumping Technologies (HPT TCP)



- Part of the **IEA HPT Project 68**
<https://heatpumpingtechnologies.org/project68/>
- Several workshops on the integration of HTHP in the sector with multiple stakeholders
 - Increase knowledge in the sector
 - More implementations in the sector
- **First Workshop (online):** October/November 2026
 - Opportunities and Barriers
 - Lectures and interactive group work

Coming soon!

Would you like to join us?

Please contact:

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Sabrina.Dusek@ait.ac.at

THANK YOU VERY MUCH

Anton Beck

Research Engineer

Sustainable Thermal Energy Systems

Austrian Institute of Technology

Anton.Beck@ait.ac.at

AHEAD – Pioneering CO₂- Free Steam Without Gas.

Refrigeration and Heat-Pump Engineer
Project manager



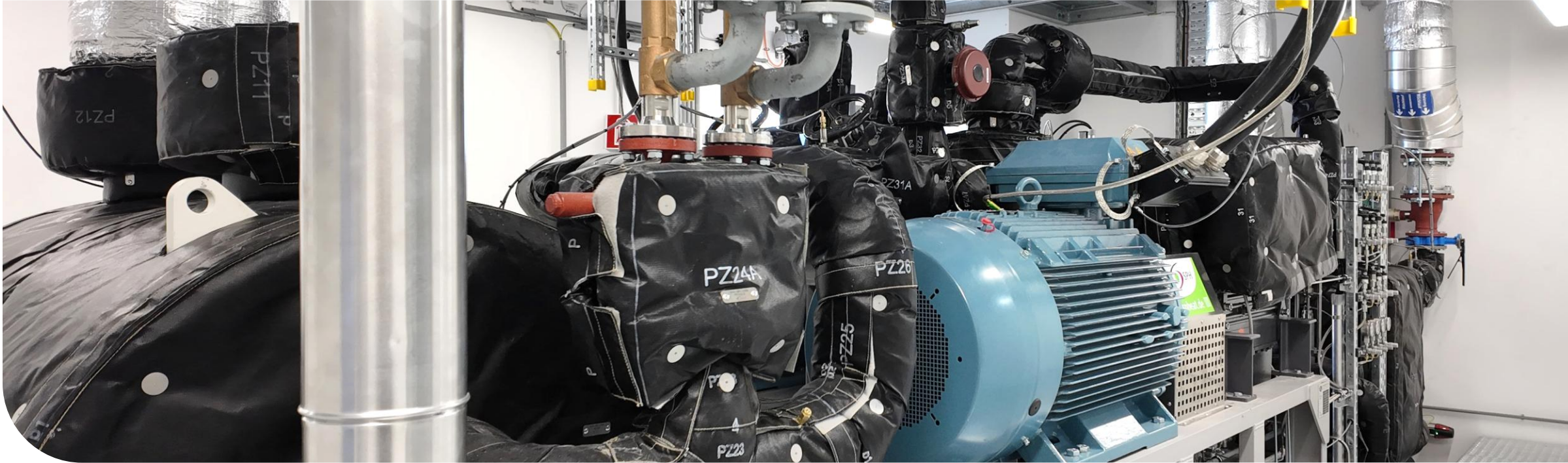


AHEAD ADVANCED HEAT PUMP DEMONSTRATOR



Better Health, Brighter Future





AHEAD - Pioneering CO₂-Free Steam without Gas

Challenges and Experiences in Producing Chilled Water (6°C), Heating Water (70°C), and Steam (184°C) with Natural Refrigerants

Doris Hofbauer

Takeda Manufacturing Austria AG, Vienna, Austria





This project has the potential
to produce steam ...

... with 184°C, 11 bar(a), 1,7 MW, 2,5 to/h

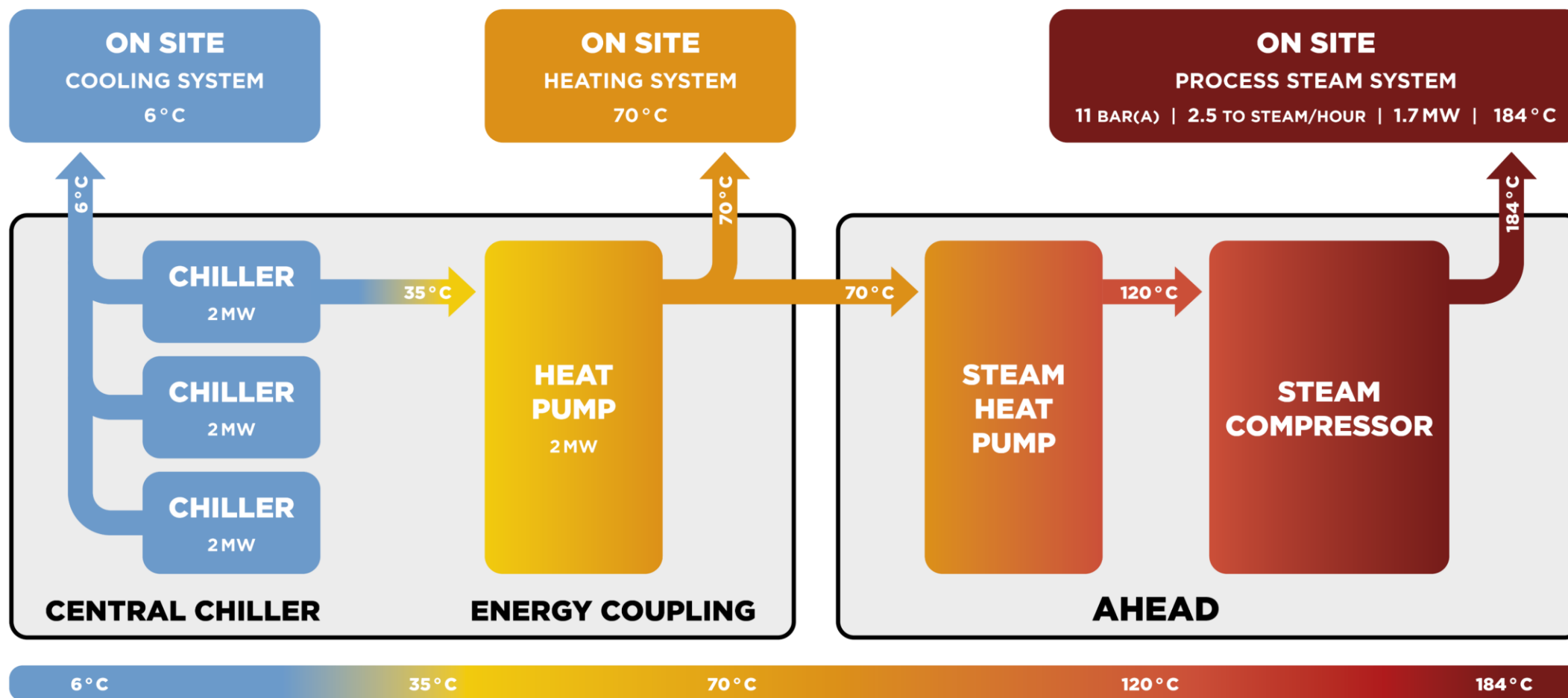
... with 100 % natural refrigerants

... with almost zero CO₂ emissions over 7 month a year on

... with up to minus 80 % greenhouse gas emissions
at Takeda's largest production site in Vienna

This project is essential for achieving site-specific and domestic Austrian goals, but it also makes a significant contribution to Takeda's net-zero GHG goal, as the project is scalable and can therefore be integrated into other locations worldwide!

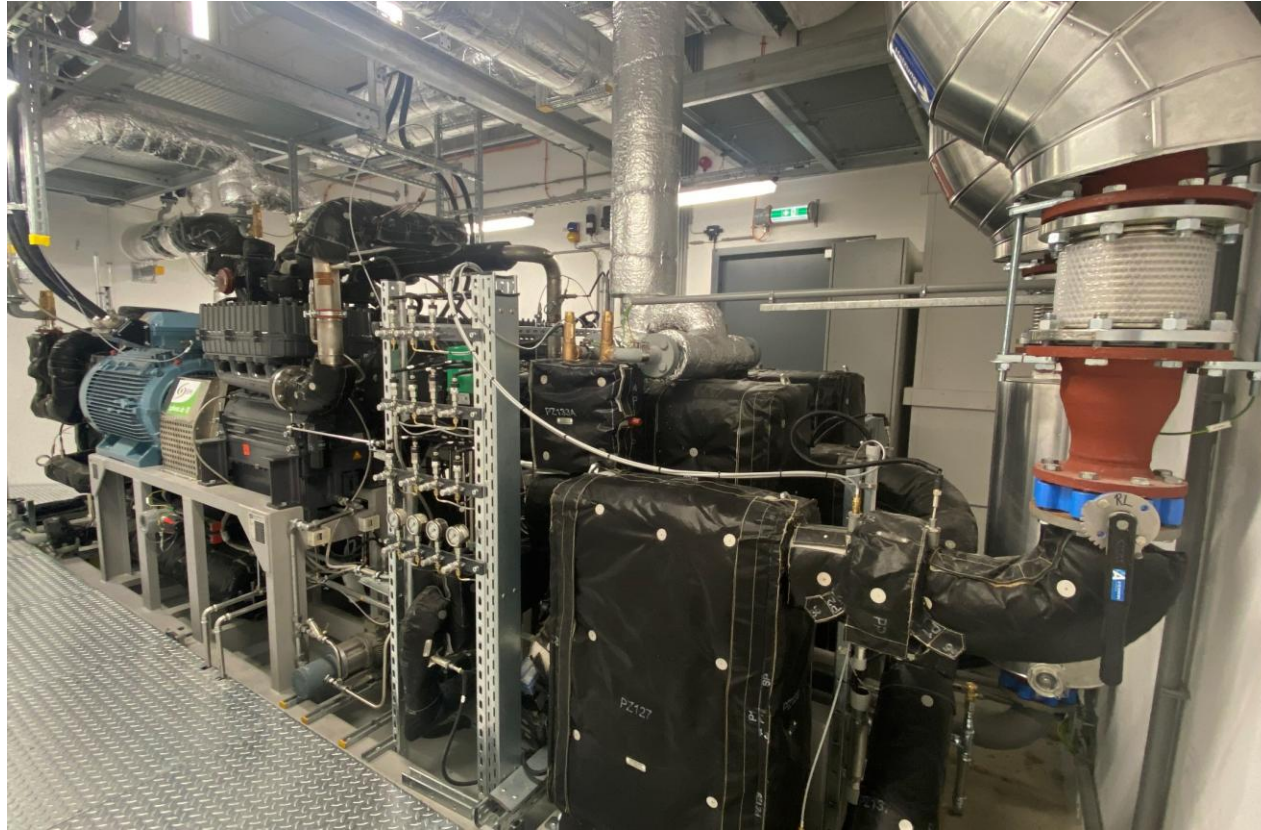
From Chilled Water (6°C) to Heating Water (70°C) and Steam (184°C)



Central Chiller (Chilled Water, 3x 2MW, 6°C, R-717) and Energy Coupling (Heating Water, 2MW, 70°C, R-717)

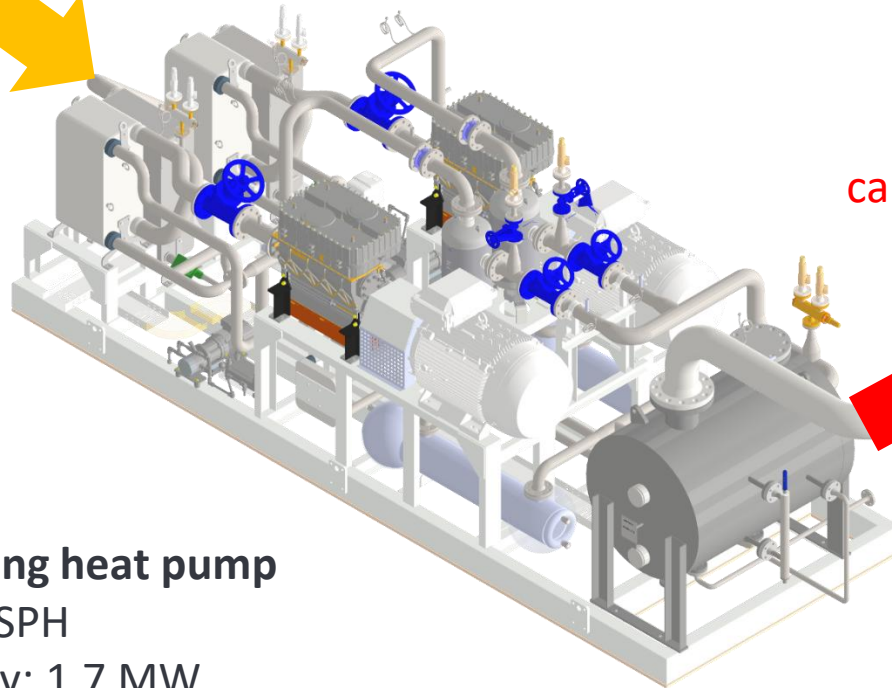


AHEAD: Heat Pump (Heating water 70°C → 120°C steam, 1,7 MW, 180 kg R-600) and steam compressor (120°C → 184°C, 2500 kg/h)



AHEAD: ADVANCED HEAT PUMP DEMONSTRATOR

warm water
70°C



Steam generating heat pump

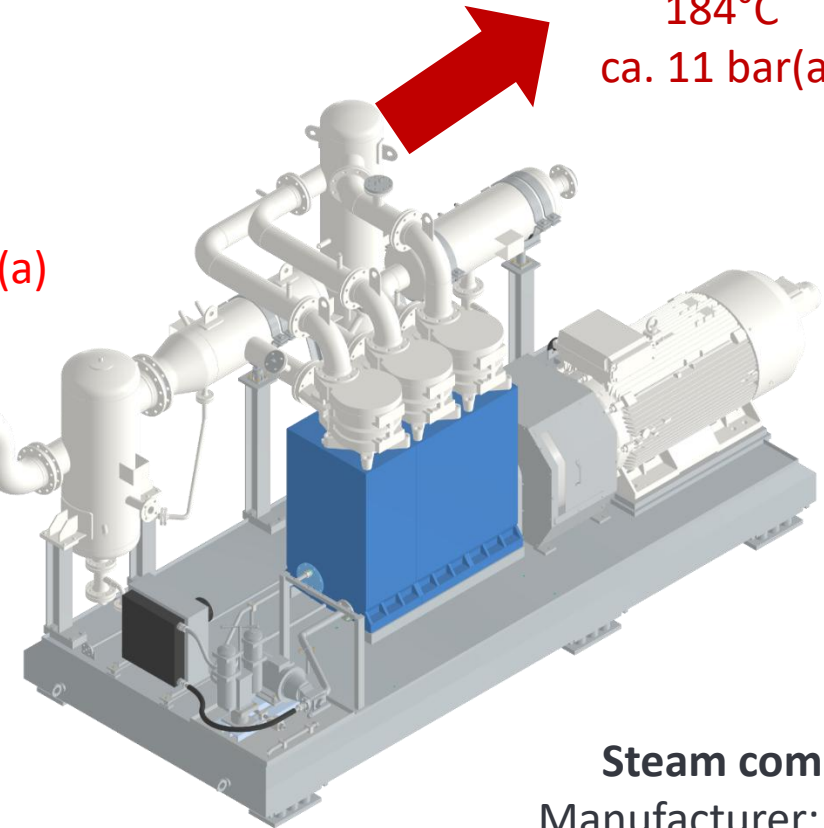
Manufacturer: SPH

Heating capacity: 1.7 MW

COP: ca. 4.4

Refrigerant: 180 kg R600 (n-butane)

steam
120°C
ca. 1,9 bar(a)



steam
184°C
ca. 11 bar(a)

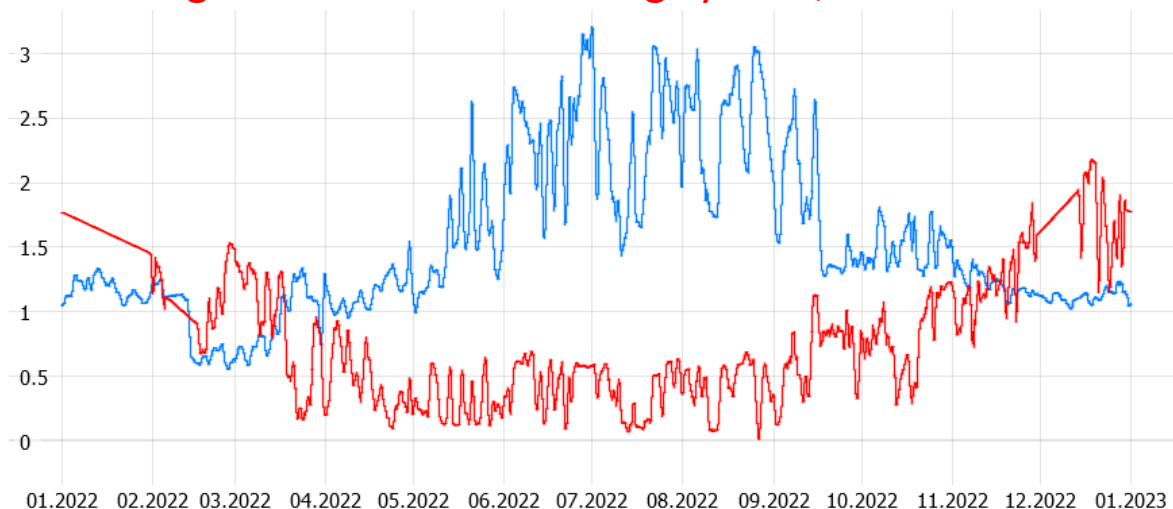
Steam compressor
Manufacturer: Spilling
Capacity: 2.5 t/h steam

Challenge: Proper operation through winter

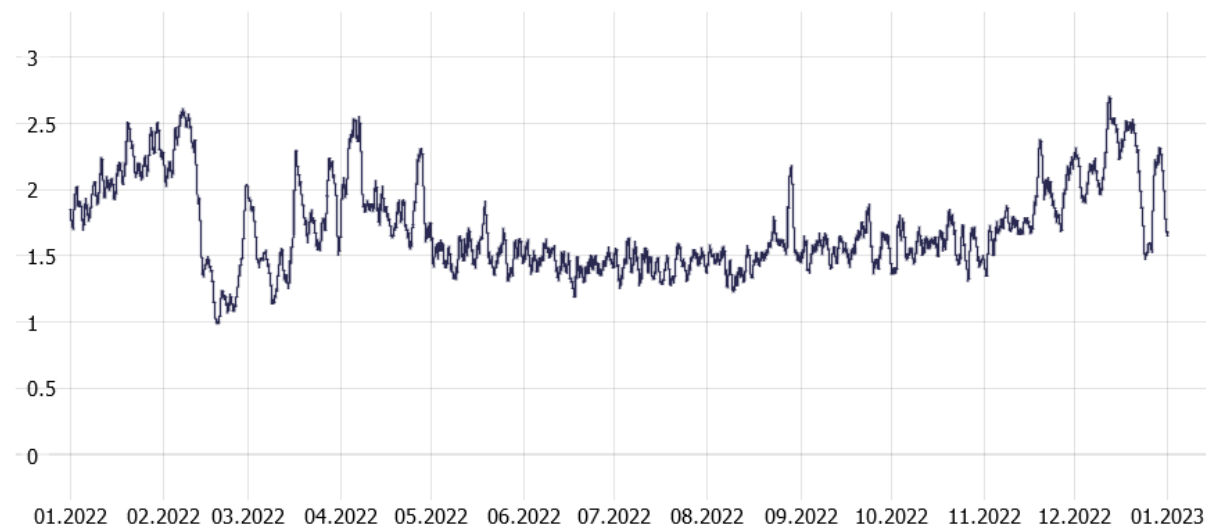


Seasonal fluctuations of sources and sinks (heating, steam demand, available waste heat from the refrigeration machines)

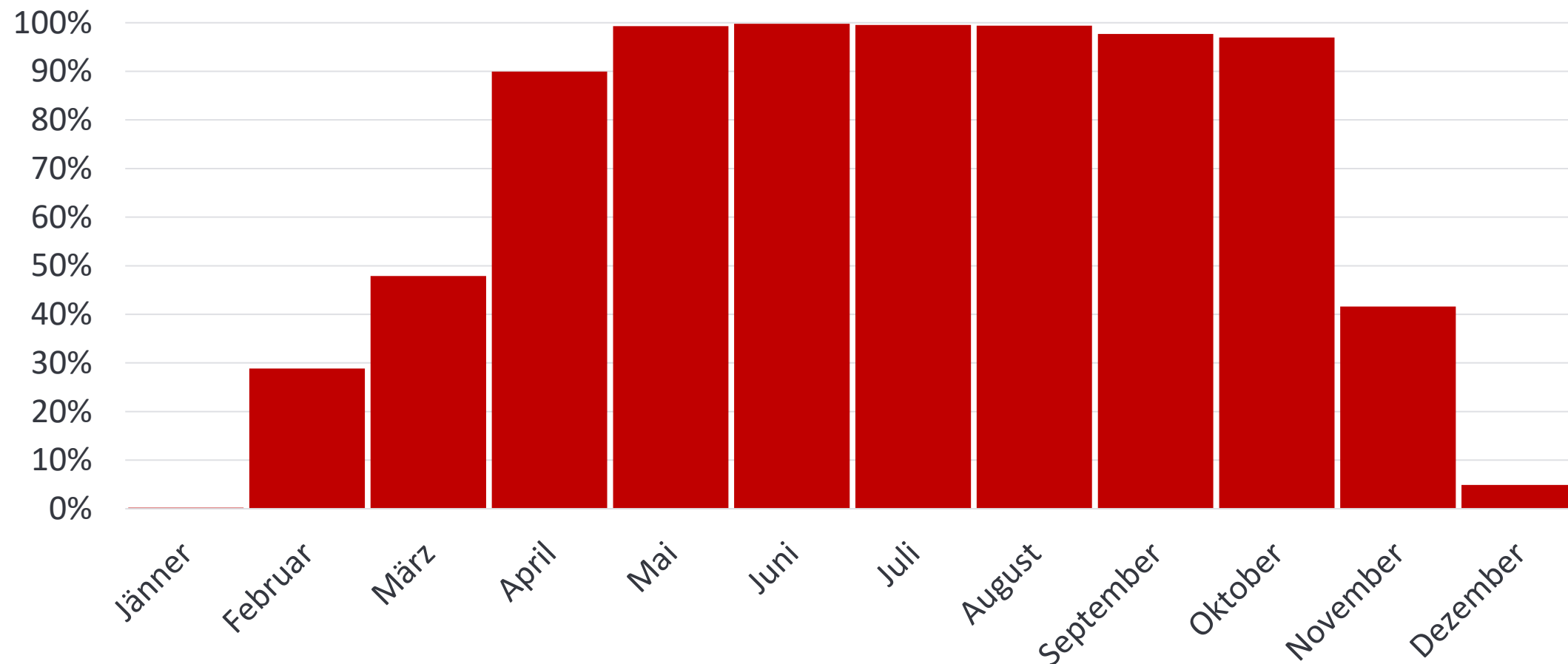
Waste heat output of the refrigeration machines, MW
Heating demand of the heating system, MW



Steam demand, t/h



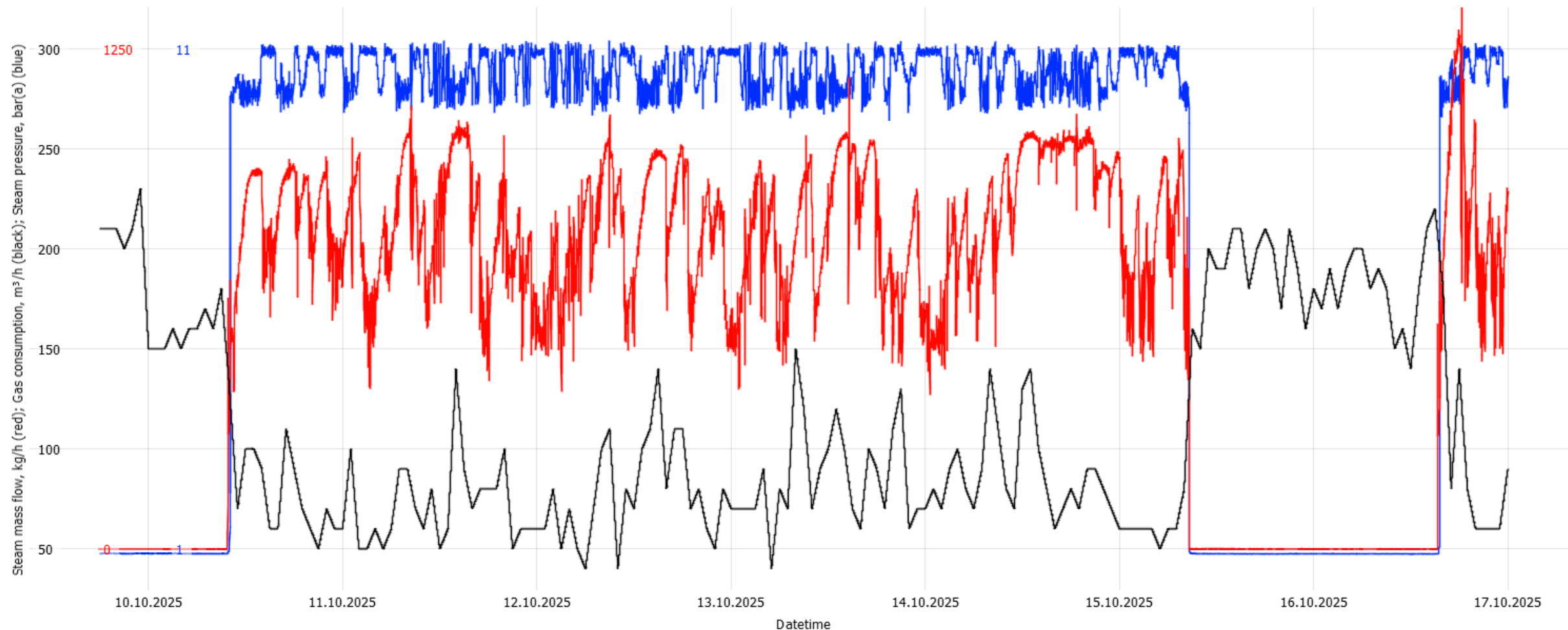
STEAM Demand covered by AHEAD (Simulation)



One week of operation in mid-October



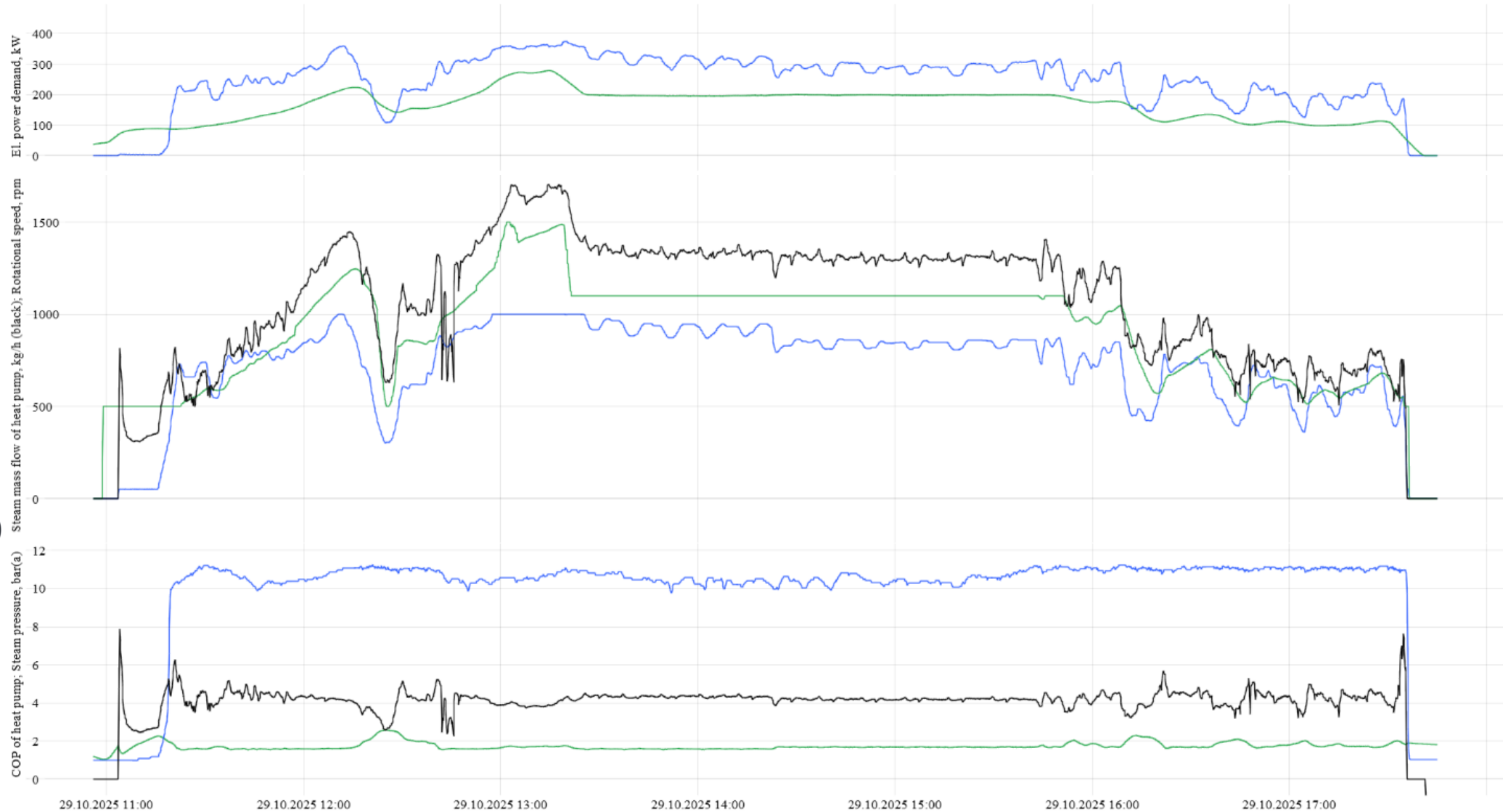
Gas consumption, m³/h (black); steam mass flow from the heat pump, kg/h (red); steam pressure from the AHEAD system, bar(a) (blue)



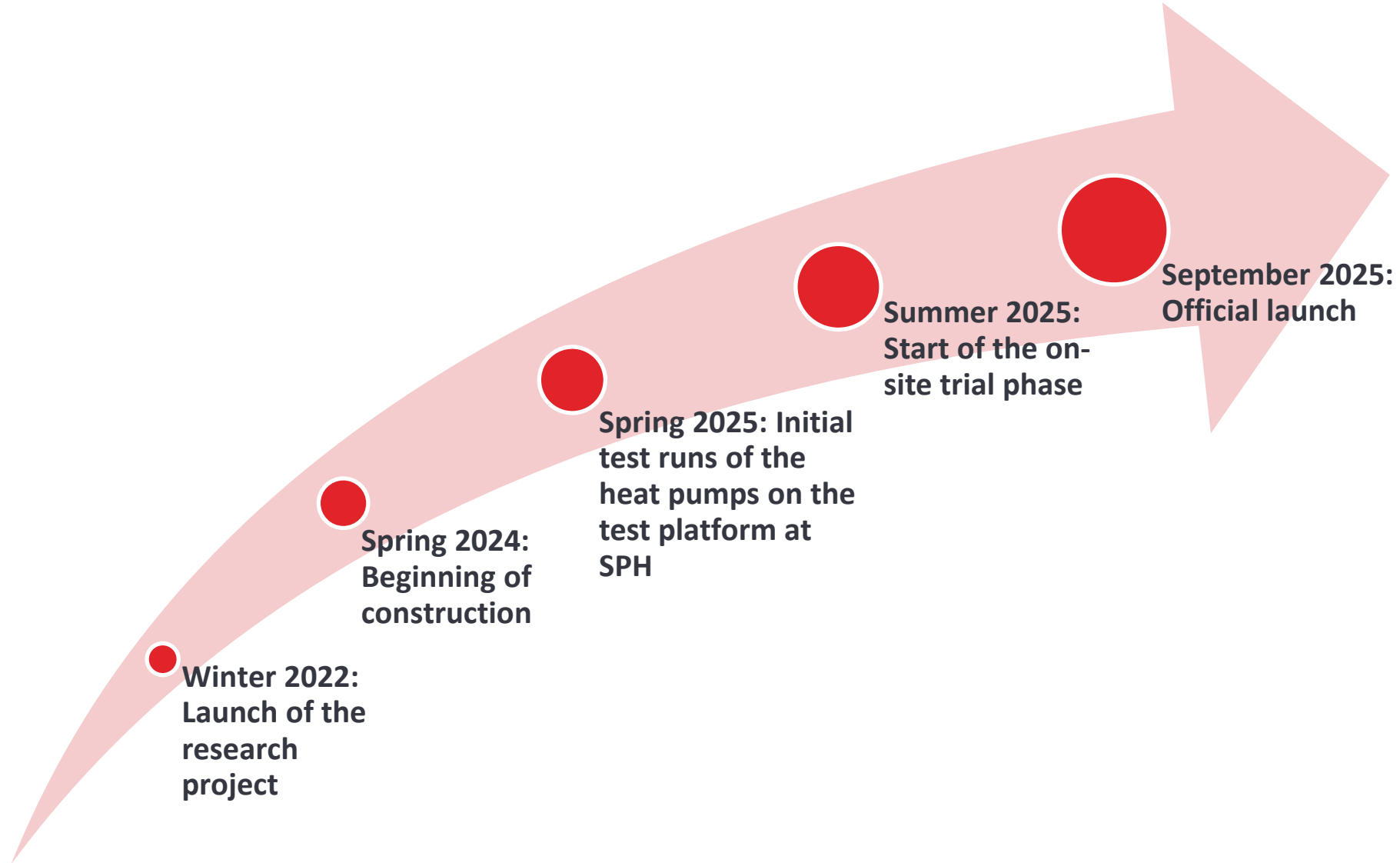
One day of operation in October



- **Electrical power demand in kW (top)**
- **Steam mass flow in kg/h (black) and rotational speeds for the heat pump and steam compressor in rpm (middle)**
- **COP (black) and steam pressure in bar(a) (bottom)**
- Colors:
SPH heat pump: green
MVR: blue



Milestones



- **limited long-term experience with large high-temperature heat pumps**
oil, seals, component lifetime
→ challenges with 2 MW R-717 heat pump
- **Complex start-up and operation of the full cascade**
(refrigeration system / 70°C heat pump / steam heat pump / steam compressor)
differences between summer and winter operation
part load vs. full load
- **Once the system is running, it runs really well**
COP even better than expected
- **Difficult to measure the real COP of the overall system**
steam flow measurement issues in the slightly superheated range
- **It only works with a strong team**
close cooperation between maintenance, engineering, suppliers and specialists

Thanks to the whole team!



Kick-off Research Project, December 2022



Kick-off Implementation Project, May 2024





This project has the potential
to produce steam ...

... with 184°C, 11 bar(a), 1,7 MW, 2,5 to/h

... with 100 % natural refrigerants

... with almost zero CO₂ emissions over 7 month a year on

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MMst. DI Harald Erös Ing. Doris Hofbauer, BSc

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Benatzkyg. 2-6, 1220 Vienna, Austria

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doris.hofbauer@takeda.com



Steam generation for pharma industry using Stirling heat pumps

Torgrim Aase
Senior R&D Engineer



Industrial High Temperature Heat Pumps for pharmaceutical decarbonization

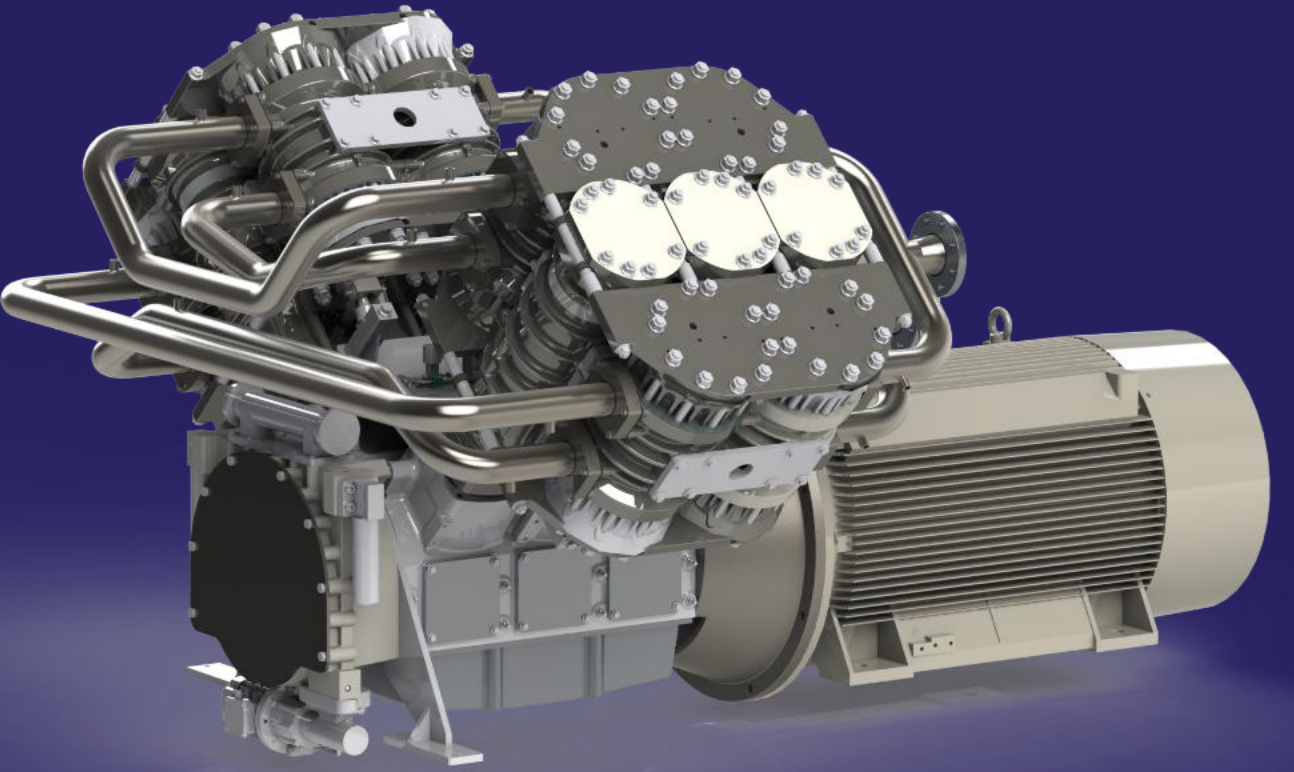
Torgrim Aase

Senior R&D Mechanical Engineer

17 September 2026

R-704 Helium:

Inert, non-toxic, zero ODP, zero GWP



400 kW industrial heat pump

- Steam or hot water up to 200°C.
- Any heat source from -30°C:
Waste heat, coolers, ambient.

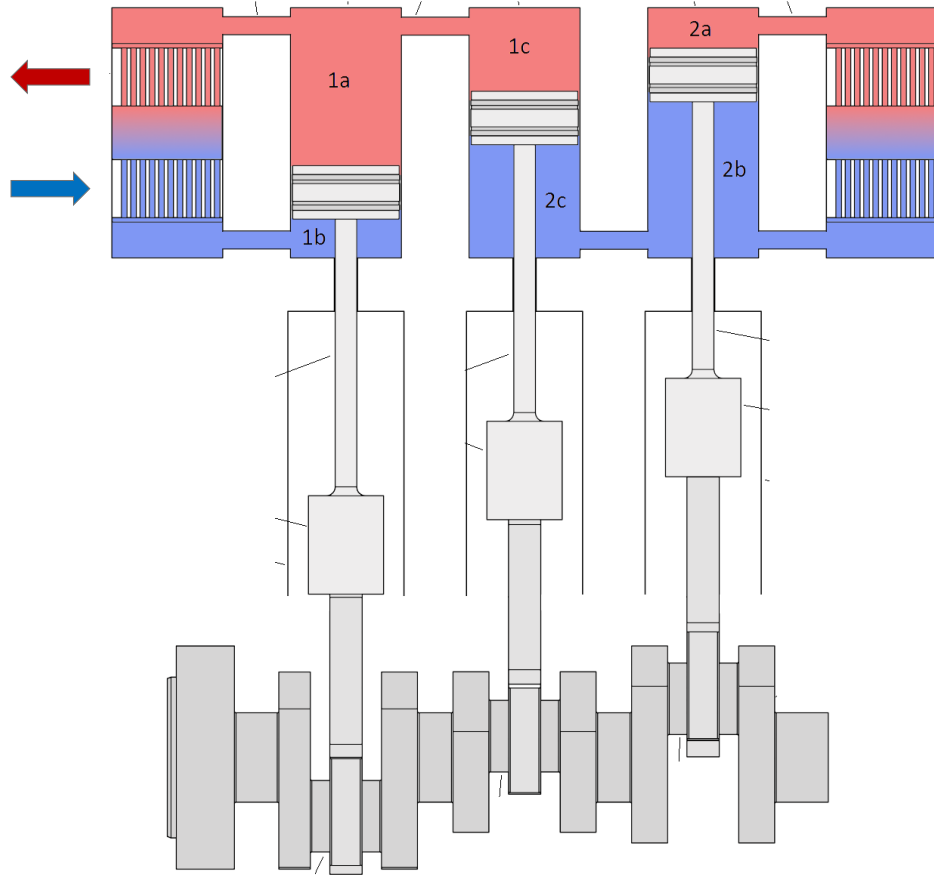
Stirling cycle

- High COP at high temperature lifts.
- Robust to varying operating conditions.
- Heating capacity not affected by temperatures.

Piston compressor with integrated heat exchangers

- Sink: Hot-water circuit to steam generator.
- Source: Cold-water circuit.
- Power: Induction motor/VFD.

Stirling-cycle heat pump layout



Power piston (mid-cylinder):

- Separates the circuits.
- Compression and expansion work.

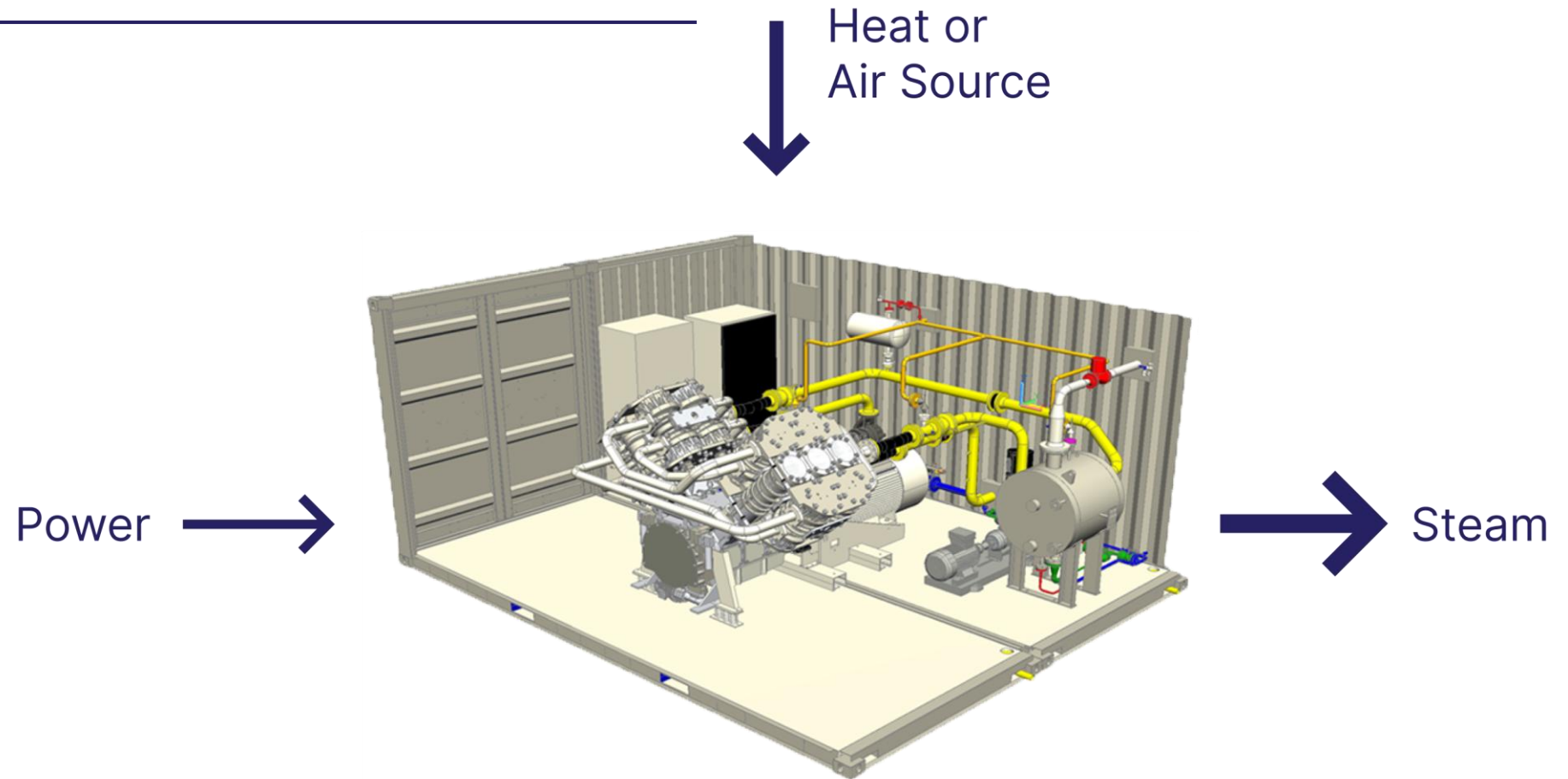
Displacer pistons:

- Moves gas through the heat exchanger. through the regenerator between the hot and cold volumes.

Heat exchangers:

- Heat hot-water circuit (sink).
- Cool cold-water circuit (source).

Simple integration — Future proof



Heat pump and steam generator

Heat pump



Steam pipe to factory

Water-heated
steam generator

Feedwater
pump

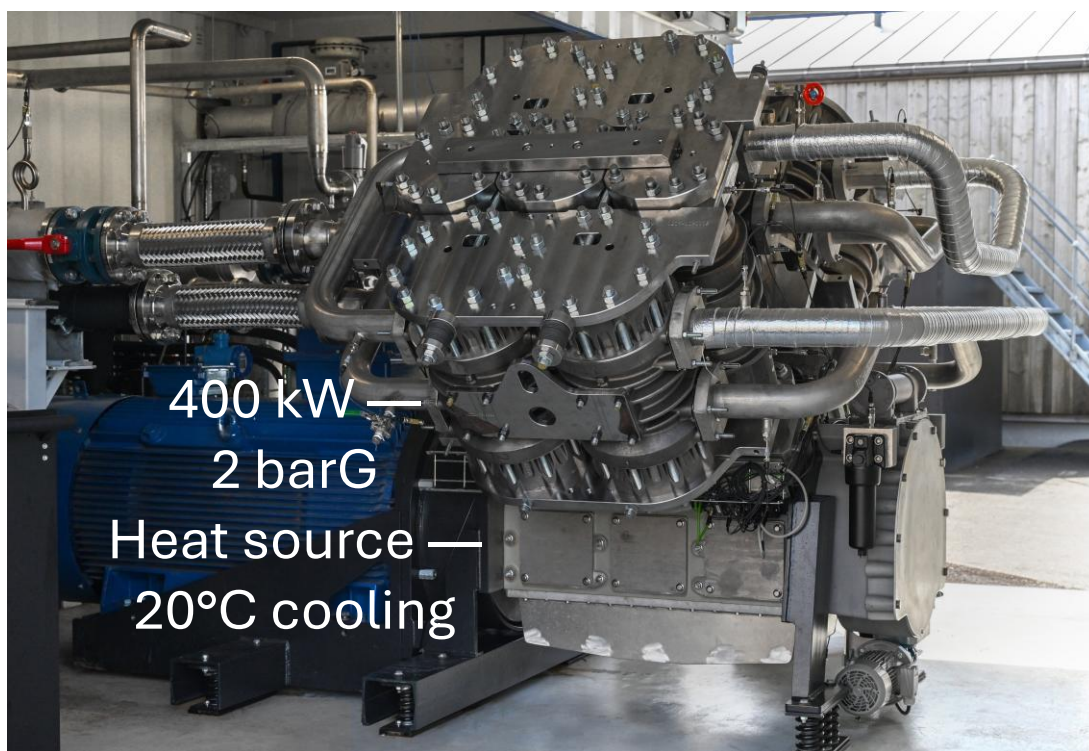
Performance data from three industrial pilots

Commercialization timeline

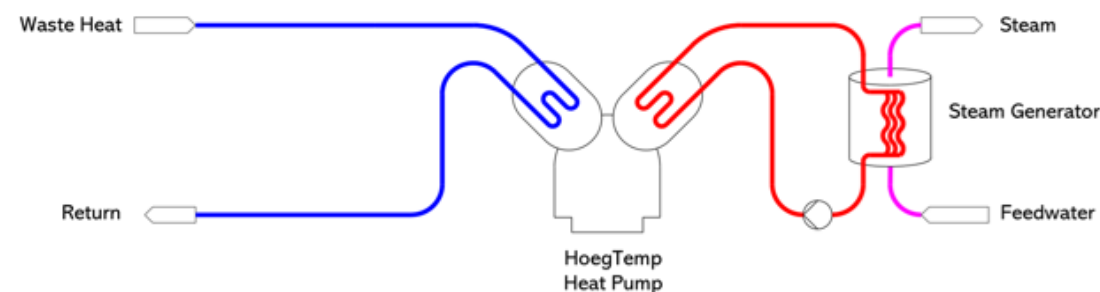


IVAR IKS Bryne — Biogas 2023

Waste heat from the cooling water circuit (21–22°C) is collected in a closed-loop water circuit (heat sink).



The heat is transferred to a steam generator, producing steam at 140–200°C for reuse in the biogas CO₂ capture process.



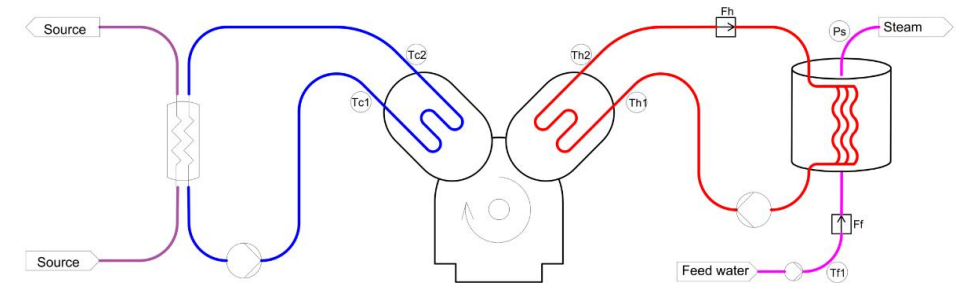
Pelagia Måløy — Fish meal & fish oil 2025

Steam used for drying fish meal in batch processing—catch dependent.
Heat source is end-of-pipe waste heat



High & varying temperatures / steam pressures with differing waste heat profiles.

- 400 kW steam at 5 barG, varying from 2 – 8 barG.
- Waste heat sourced from 15°C – 90 °C.
- Heat delivery at 130°C – 180°C.





GE Healthcare Lindesnes

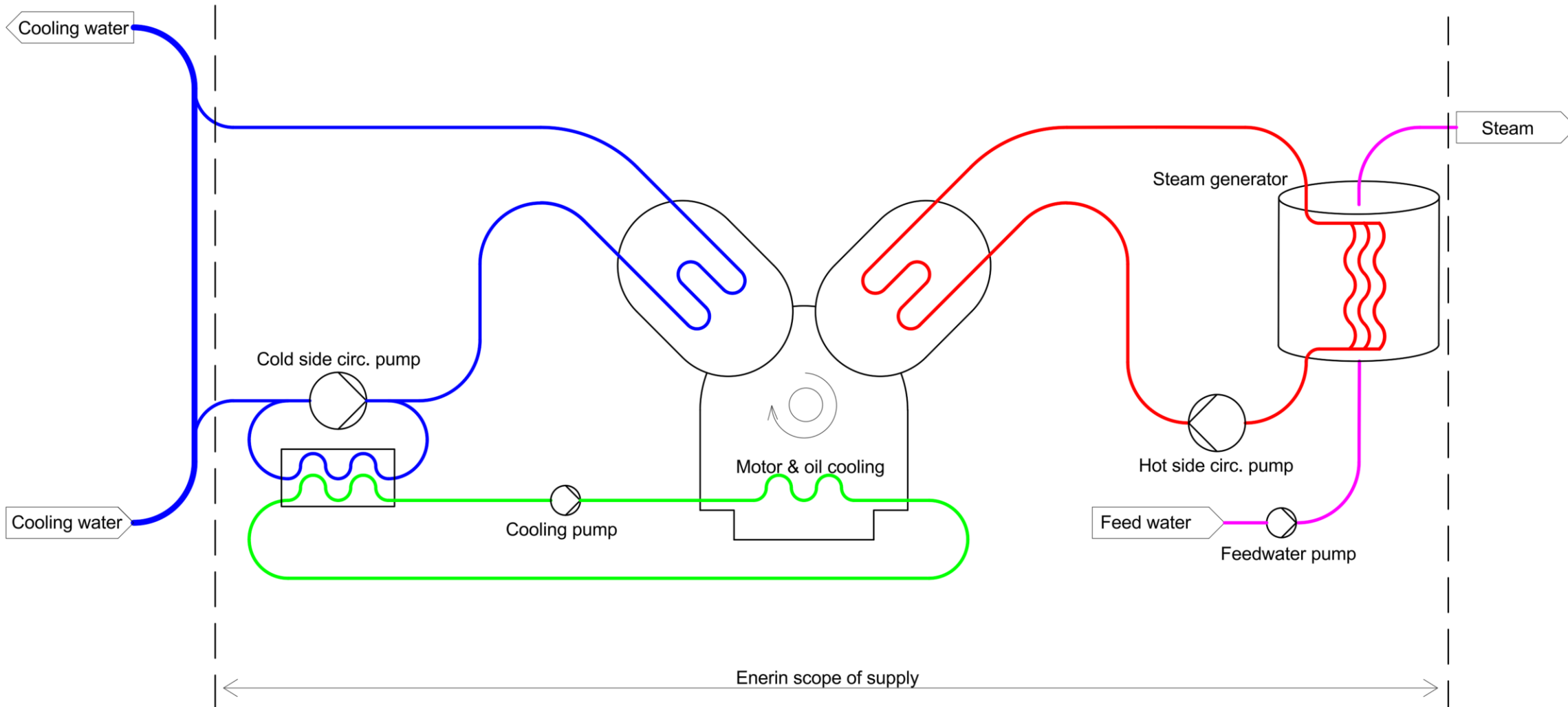
Pharmaceuticals 2024

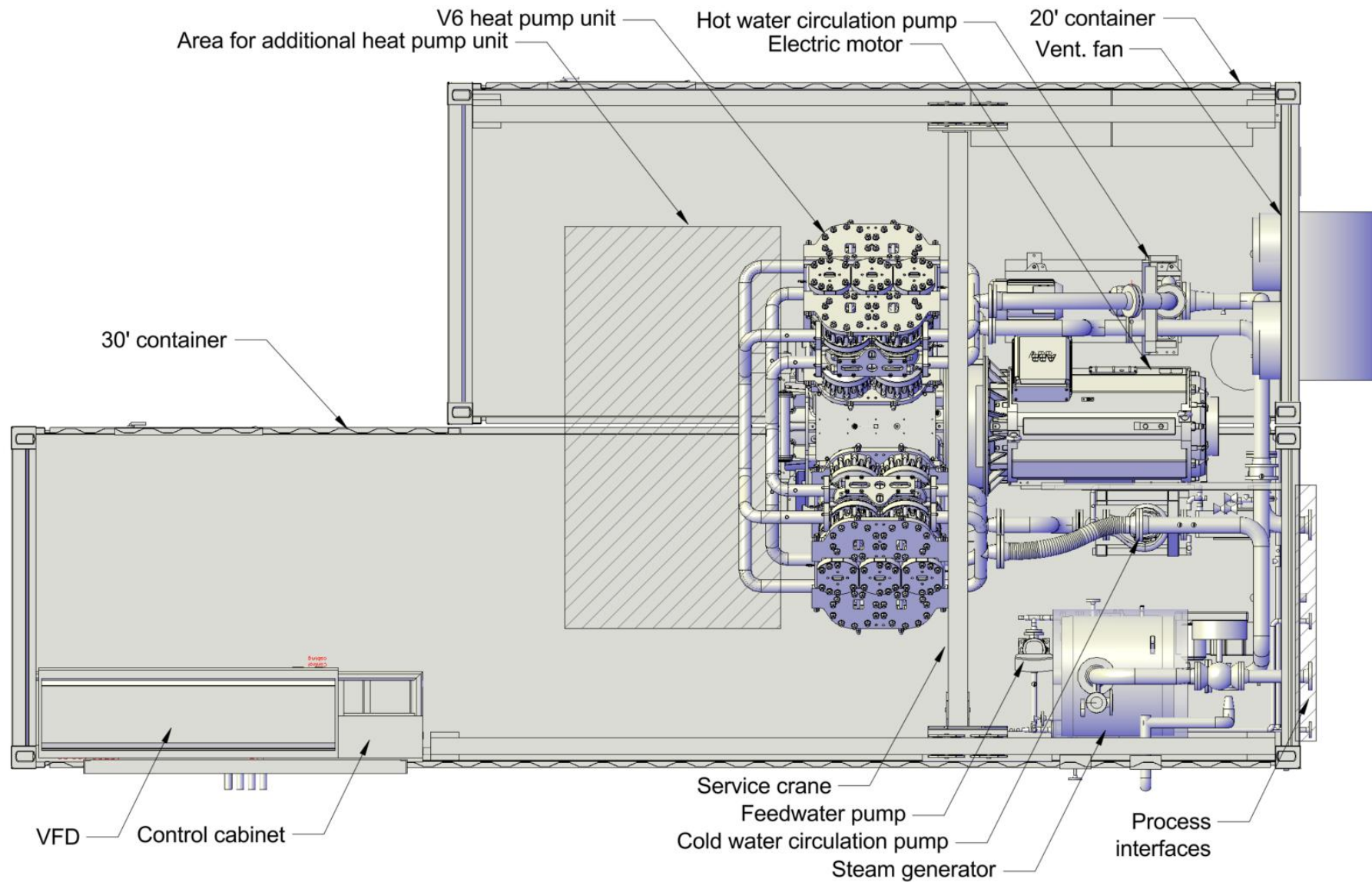
400 kW steam 2 bar_G

Heat source: 25°C cooling circuit

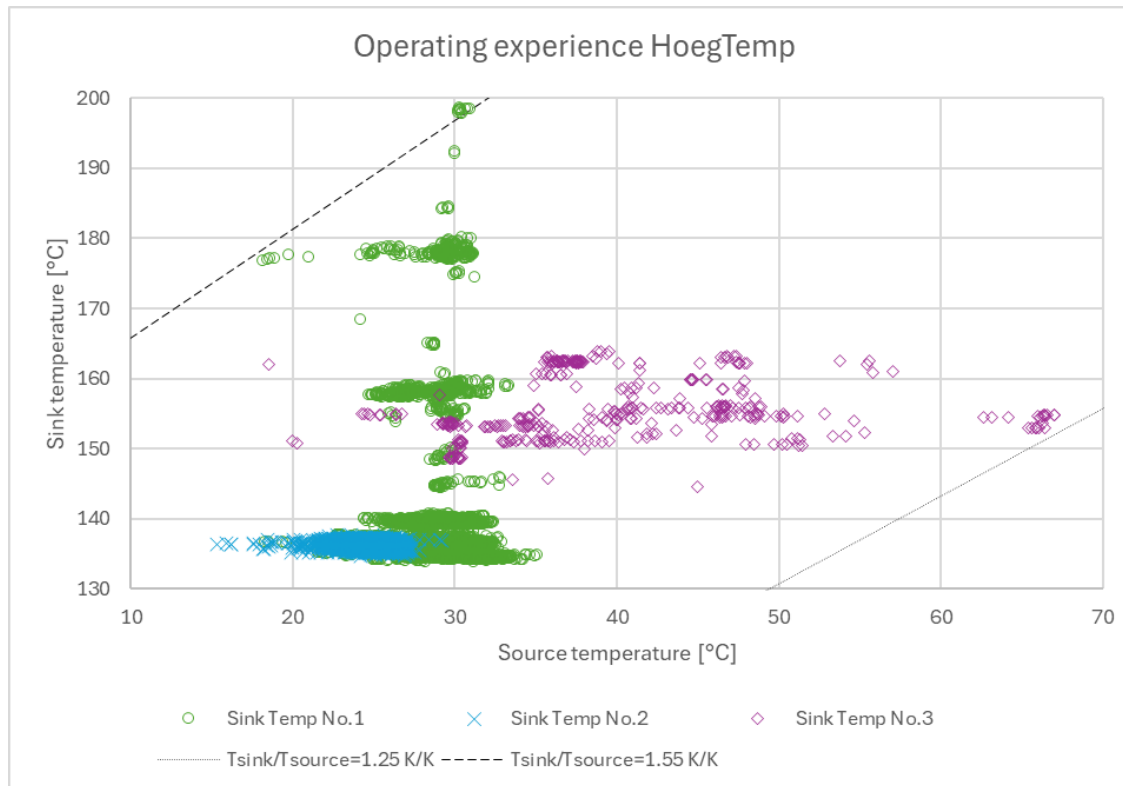


ENOVA





Different temperatures – one design



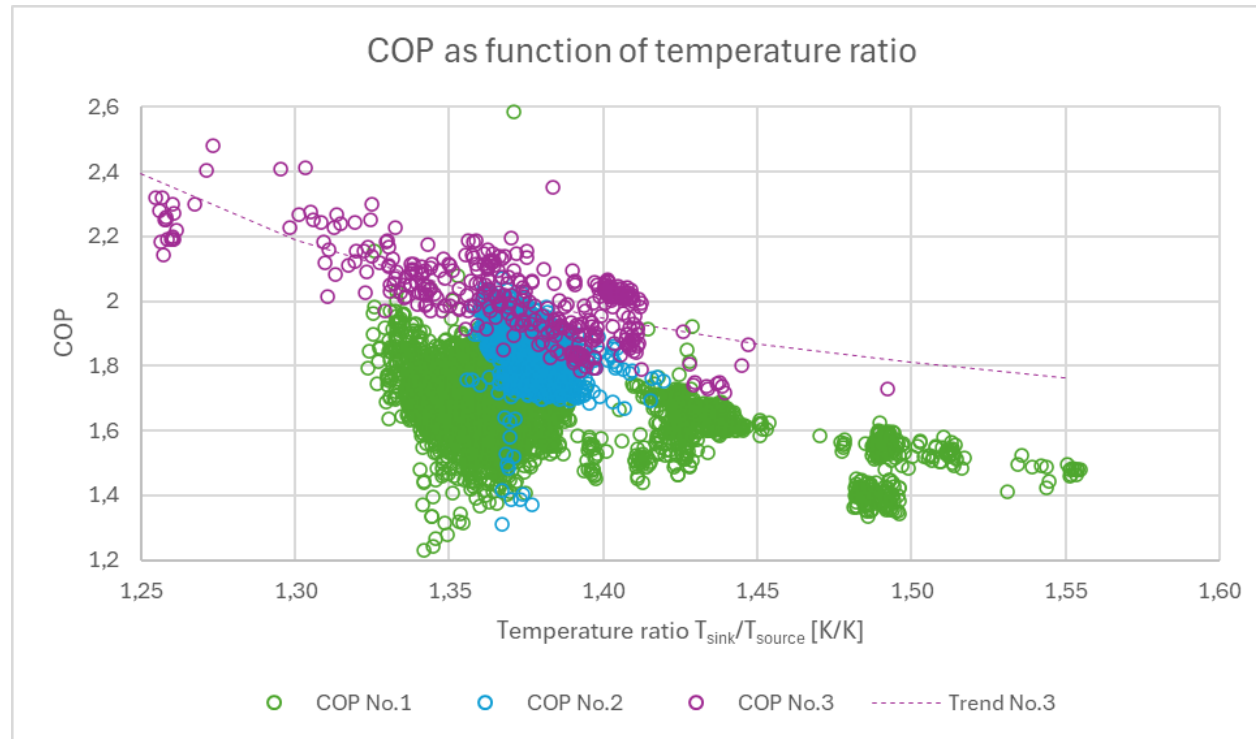
- Data analysed from the 8,000 hours with the most stable operating conditions.
- 15,000 hours as of Nov, 2025.
- Three different scenarios: tested at high, fluctuating and stable temperatures.
- Source temperatures from 15°C to 68°C.
- Sink temperatures from 134°C to 199°C (200°C/198°C circuit).

IVAR

GE Healthcare

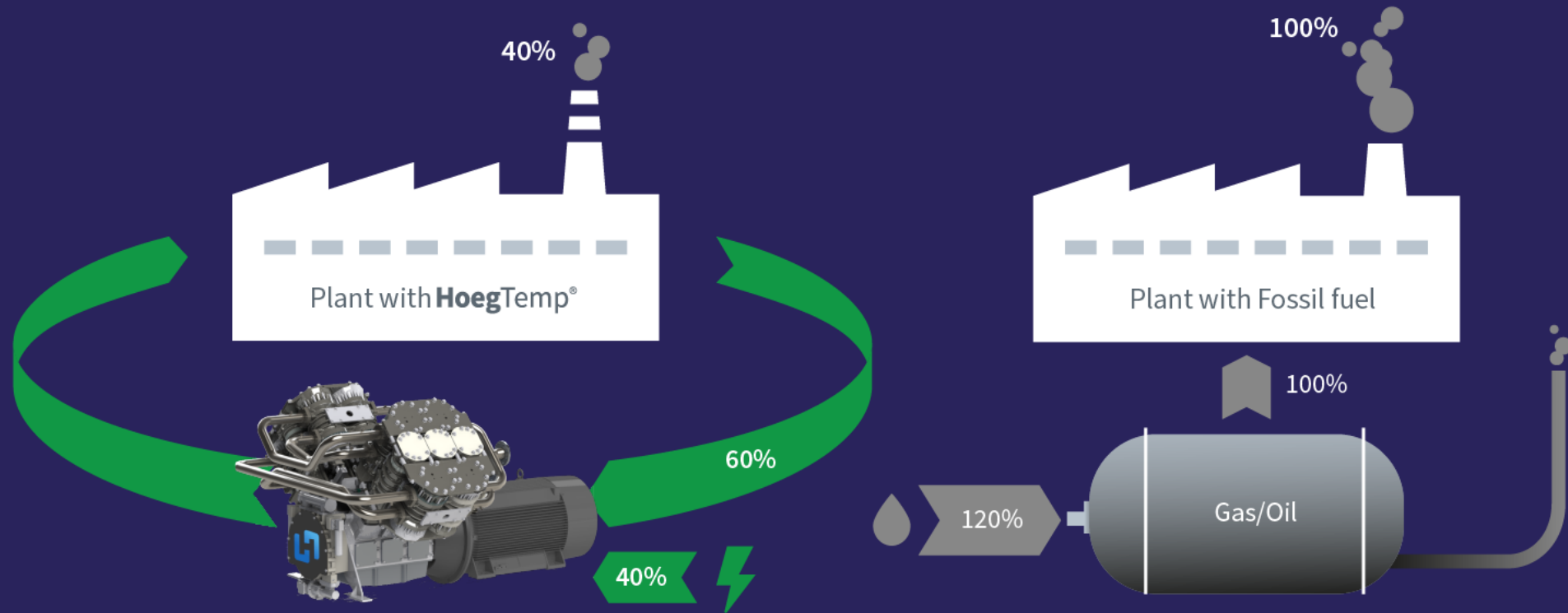
Pelagia

COP increased through minor updates



- COP a function of temperature ratio (K/K).
- GE Healthcare (blue): Modified pistons.
- Pelagia (purple): Modified heat exchangers.
- Different motor/VFD combinations — drive train efficiency excluded from charts comparing the three heat pumps.

HoegTemp vs. Fossil boiler



- 50 – 70% lower consumption
- Lower cost integration

- High cost price vulnerability
- Strain on cooling system
- Emissions

Decarbonization concepts for pharmaceutical production sites

Kurt Engelbrecht
Senior Consultant



High temperature heat pumps in the pharma industry – learnings from CHASE

IEA P68 Webinar

17 September, 2026

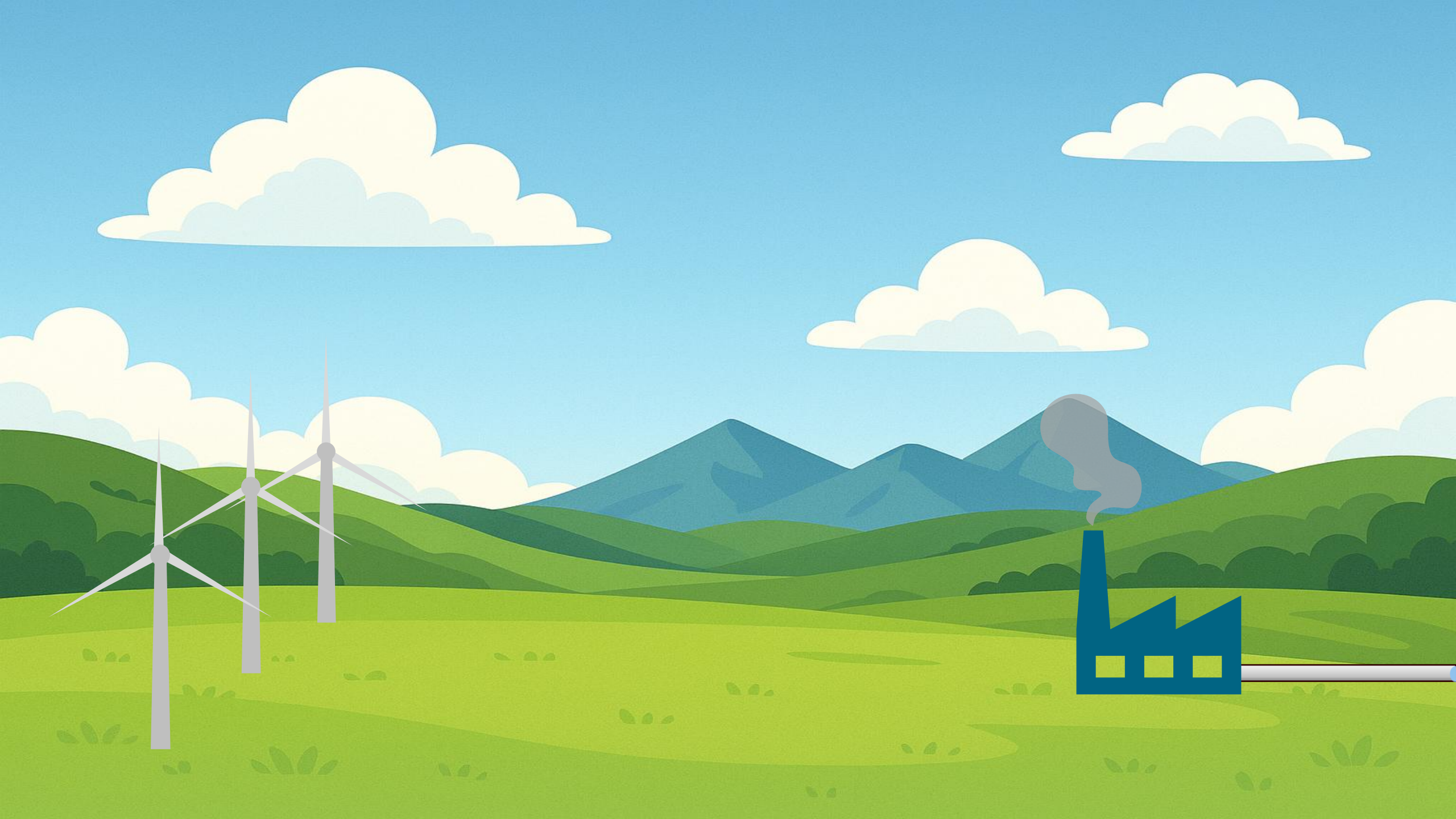
Kurt Engelbrecht

Francesco D'Ettorre

Wiebke Brix Markussn

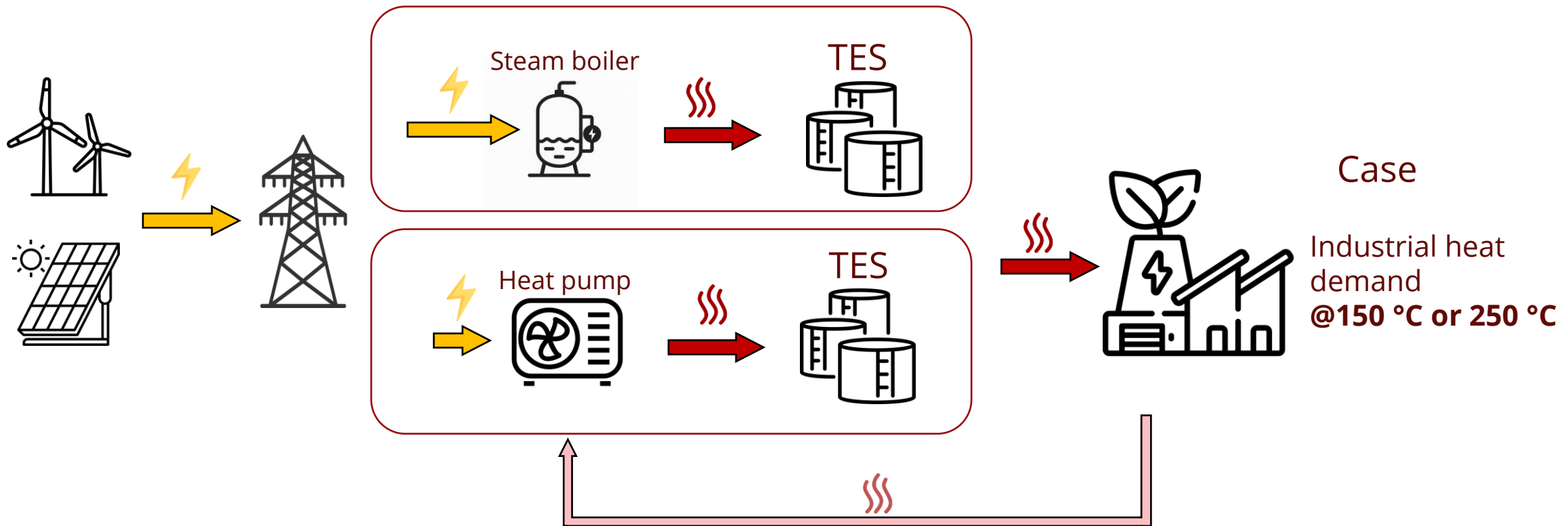
Morten Herget Christensen





CHASE project foundation

Options investigated in this study
as part of the CHASE project:



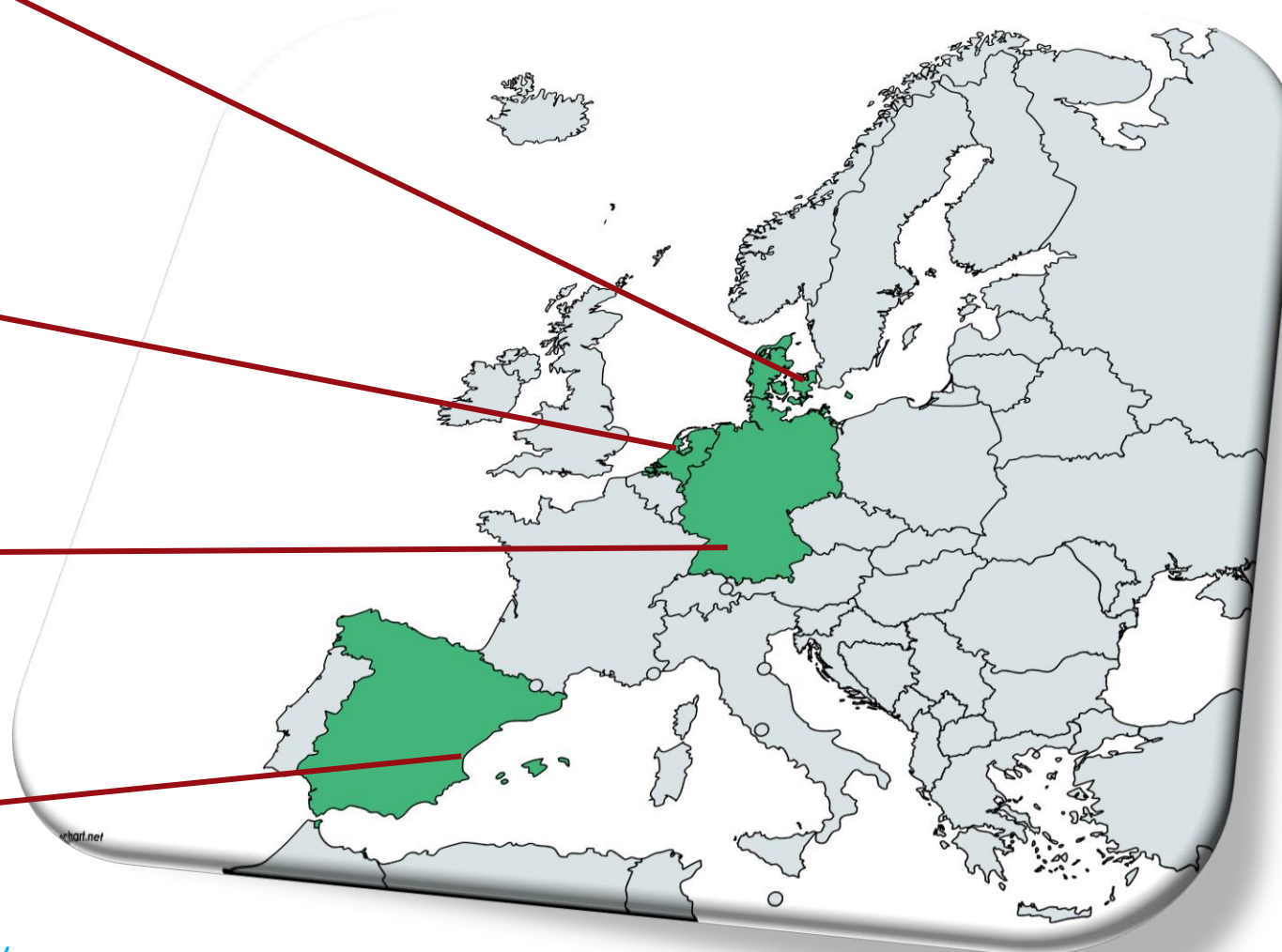
CHASE partners



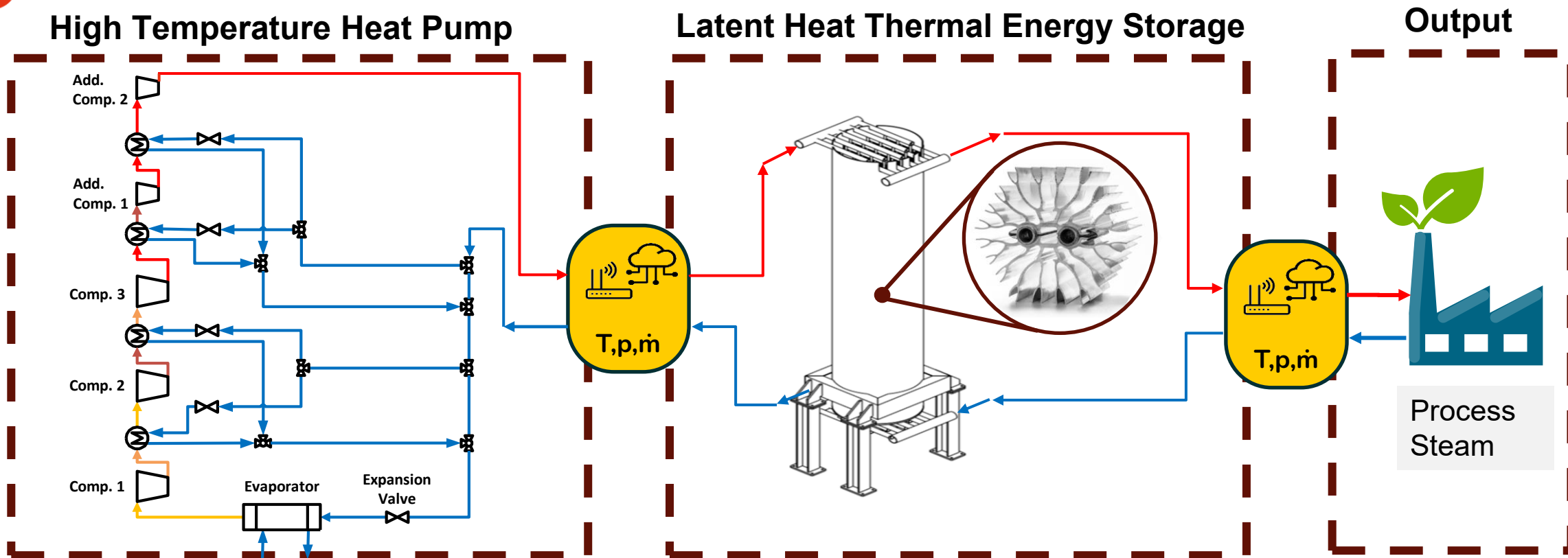
Standard Fasel



UNIVERSITAT
POLITÈCNICA
DE VALÈNCIA



(Digital) Coupling of HTHP2 and LHTES2 to CS2



(Digital) Coupling of HTHP2 and LHTES2 to CS2



High Temperature Heat Pump

- Steam compression heat pump
- 5-stage turbo compression design
- Outlet of 5th stage: 250 °C/39.8 bar
- Direct driven geared at 120 k rpm

Project CHASE:

- Physical implementation of 4th stage, simulative implementation of 5th stage



Latent Heat Thermal Energy Storage

- 1.6 tons of NaNO₃/KNO₃ (eu) as PCM, melting point: 222 °C
- Use of 19 dual-tube aluminum fins
- Charging and discharging with temperature difference <10 K
- Flexible steam up to 20 bar
- Heat storage capacity ≈ 60 kWh
- Experimental characterization of the storage within laboratory



Output

- Provided by DTI
- Simulative coupling
- Tailored to industrial requirements

Pharma use case



- Hourly steam consumption data from a relevant industrial steam user
- Production plant steam, or black steam, for general production
- Continuous steam demand over 8000 h/year
- Security of supply is extremely important
- Reducing cost of heat is an important objective
- Variation in load can be detrimental to some equipment in the steam production

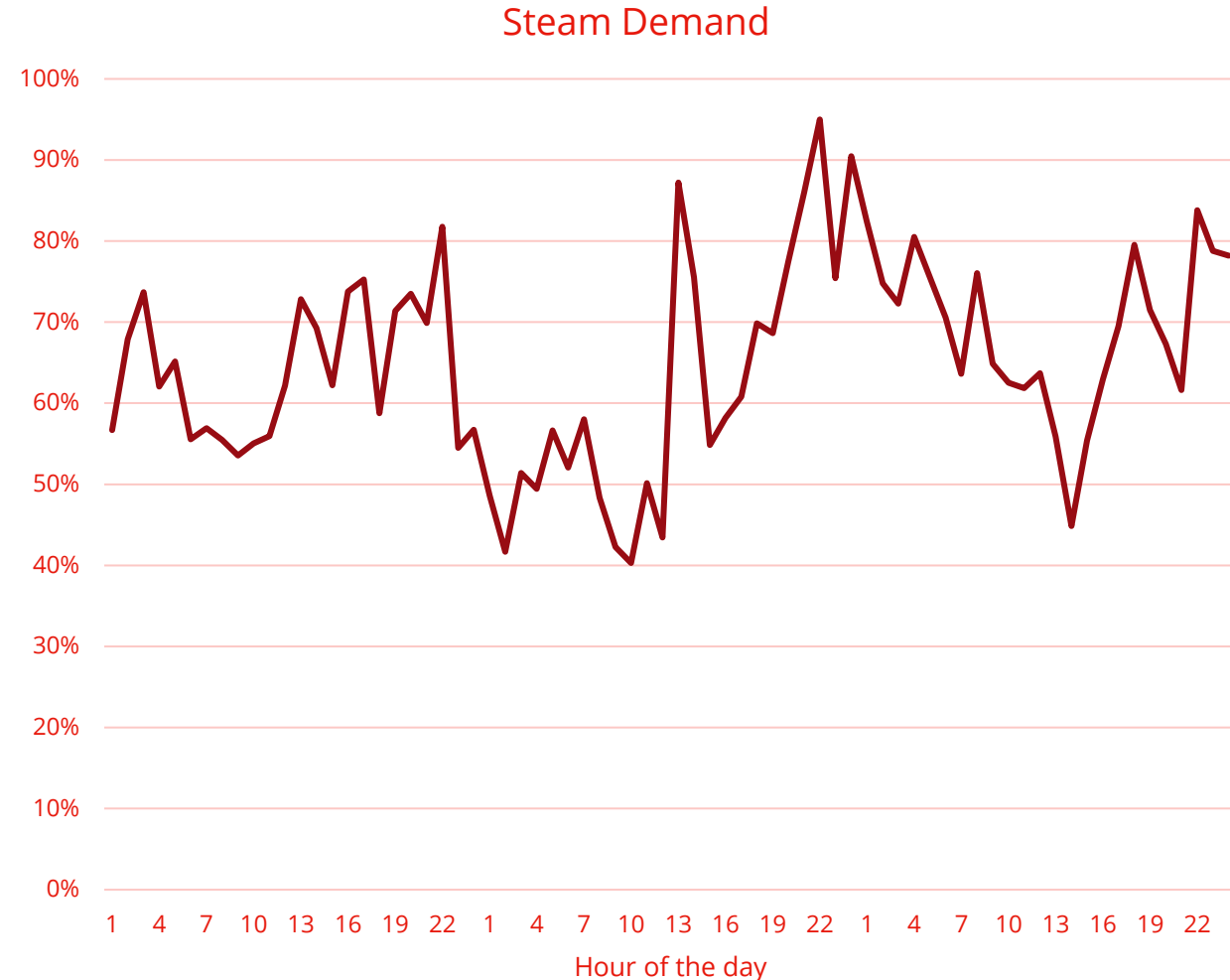


Optimization case



We have considered full year operation for a representative steam load. The data foundation is:

- 2024 electricity spot price, DSO and TSO tariffs in Denmark, the Netherlands and Spain
- Equipment CAPEX estimates
- Heat pump coupled to a thermal storage
 - Heat pump used to charge the thermal storage
- Optimization inputs
 - Heat pump COP = 1.9
 - Discount rate = 5%
 - Gas price, including tariffs and delivery = €95/MWh



Optimization approach



System configuration:

HP and TES replacing existing steam generation.
Existing generation used for peak loads

Objective function:

Minimize OPEX (Maximize net present value)

Optimization approach

Nested optimization

- Inner problem: operational optimization (MILP)
- Outer problem: exhaustive search over system sizes (HP, TES)

Optimization study: Economic tool

 NN Analysis Suite

Select Tool

☐ Energy System Analysis

☒ NPV Calculator

Model Parameters

Start Year

2026

-

+

Tax Rate (%)

22

0

50

WACC (%)

7

1

20

Inflation Rate (%)

2.00

0.00

10.00

Horizon Years

20

1

30

 NPV Business Case Calculator

Calculate the Net Present Value (NPV) of your business case over a 10-year horizon to determine if your investment creates or destroys value.

 Quick Input

 One-Time Items

 Detailed Input

 Results

 Help & Concepts

Quick Input Mode

Enter summarized values for recurring costs and savings.

Investments & Recurring Costs

Equipment Investment

Total Equipment Investment (DKK million)

15,00

Investment Years (Equipment)

2026

Equipment Ready Year

None

Apply discount rate to equipment investment?

Building Investment

Total Building Investment (DKK million)

0,00

Investment Years (Building)

Recurring Savings

Equipment Investment Savings

Annual Equipment Investment Savings (DKK million)

0,00

Investment Years (Equipment)

2026

Savings Start Year

2026

Depreciation Ready Year

Choose an option

Apply discount rate to equipment investment savings?

Building Investment Savings

Annual Building Investment Savings (DKK million)

0,00

Investment Years (Building)

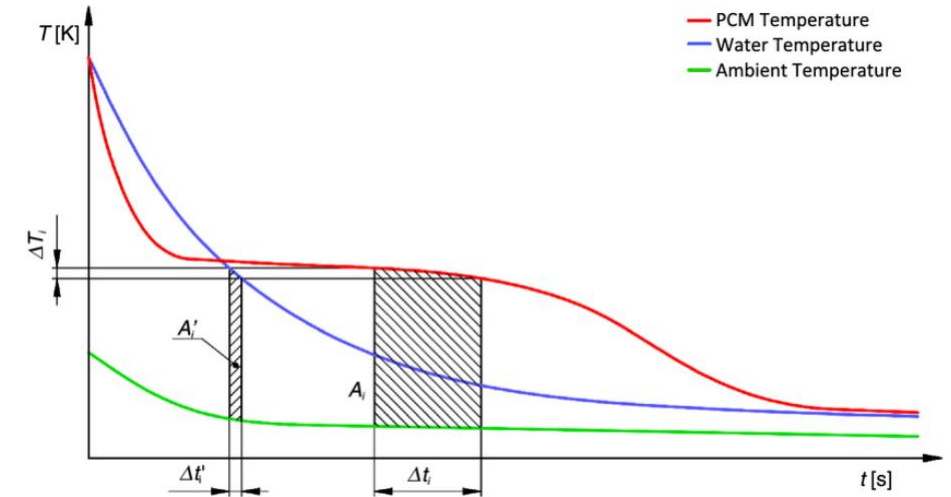
Deploy

Equipment characteristics

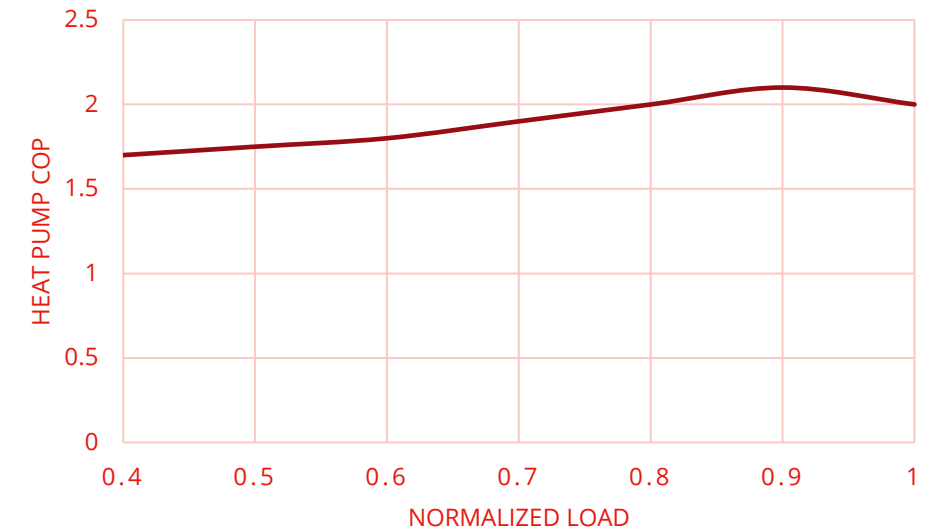
Device characteristics can be added to the MILP model

- Heat pump COP vs load
- Heat pump COP vs hot and cold temperatures
- LHTES charge/discharge curves
- LHTES efficiency as a function of SOC

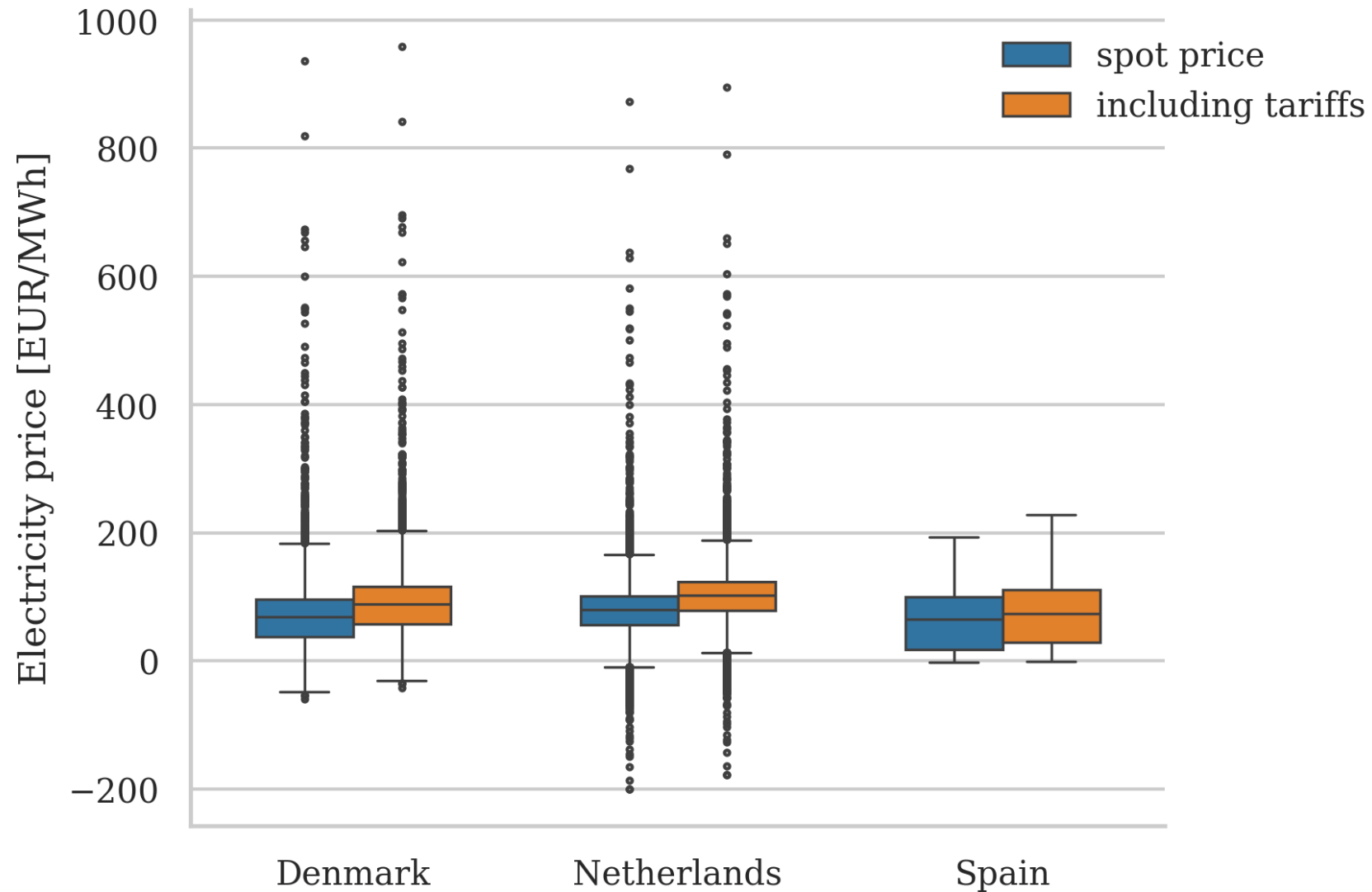
These activities are an ongoing collaboration with the Technical University of Valencia (UPV)



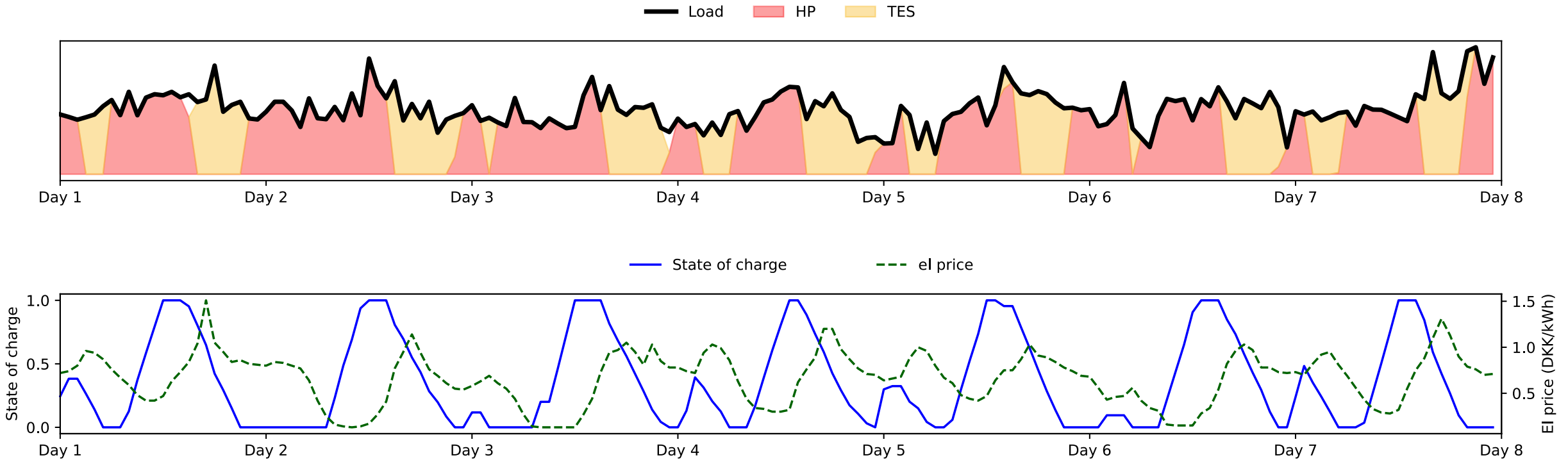
DOI: [10.1038/s41598-021-02705-1](https://doi.org/10.1038/s41598-021-02705-1)



Electricity markets

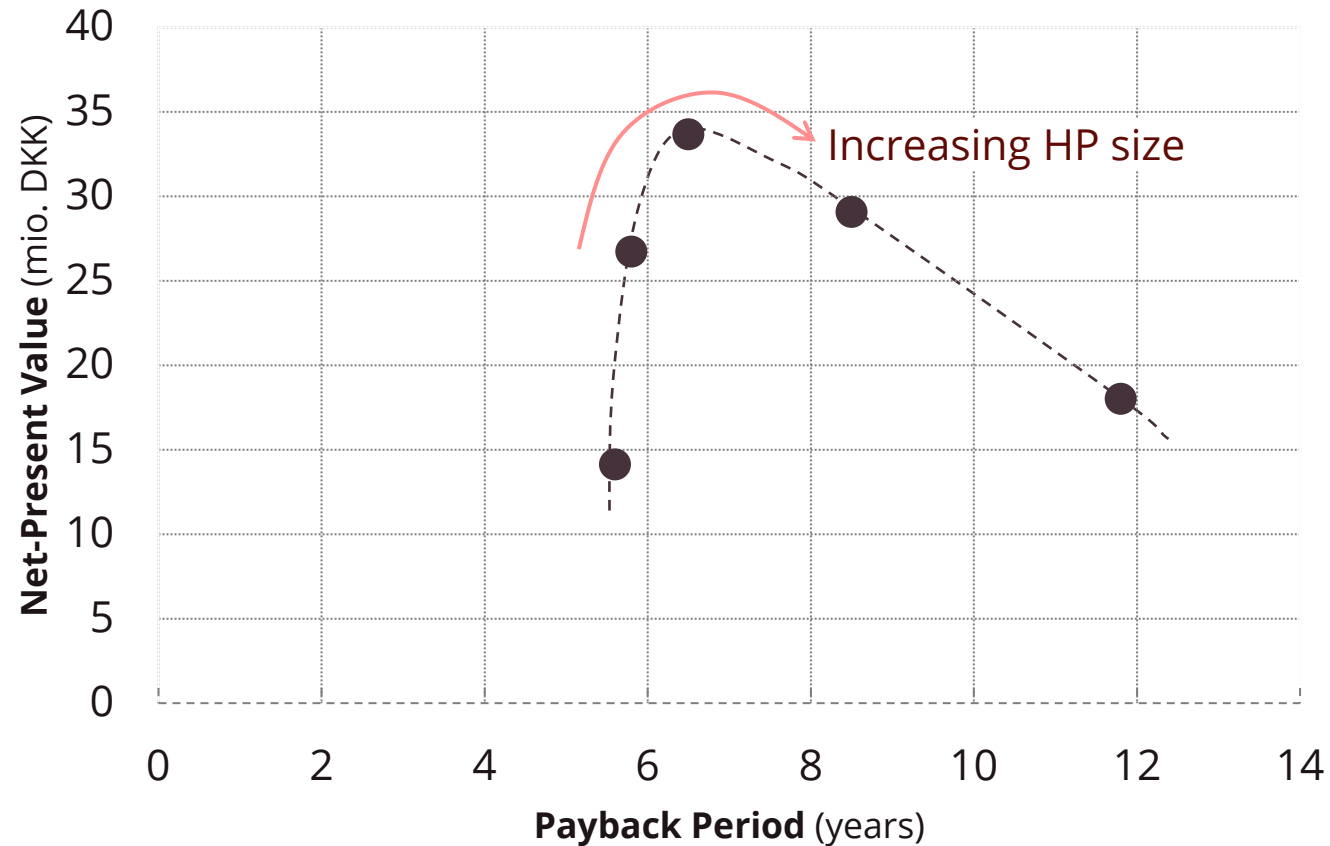


OPEX minimization example



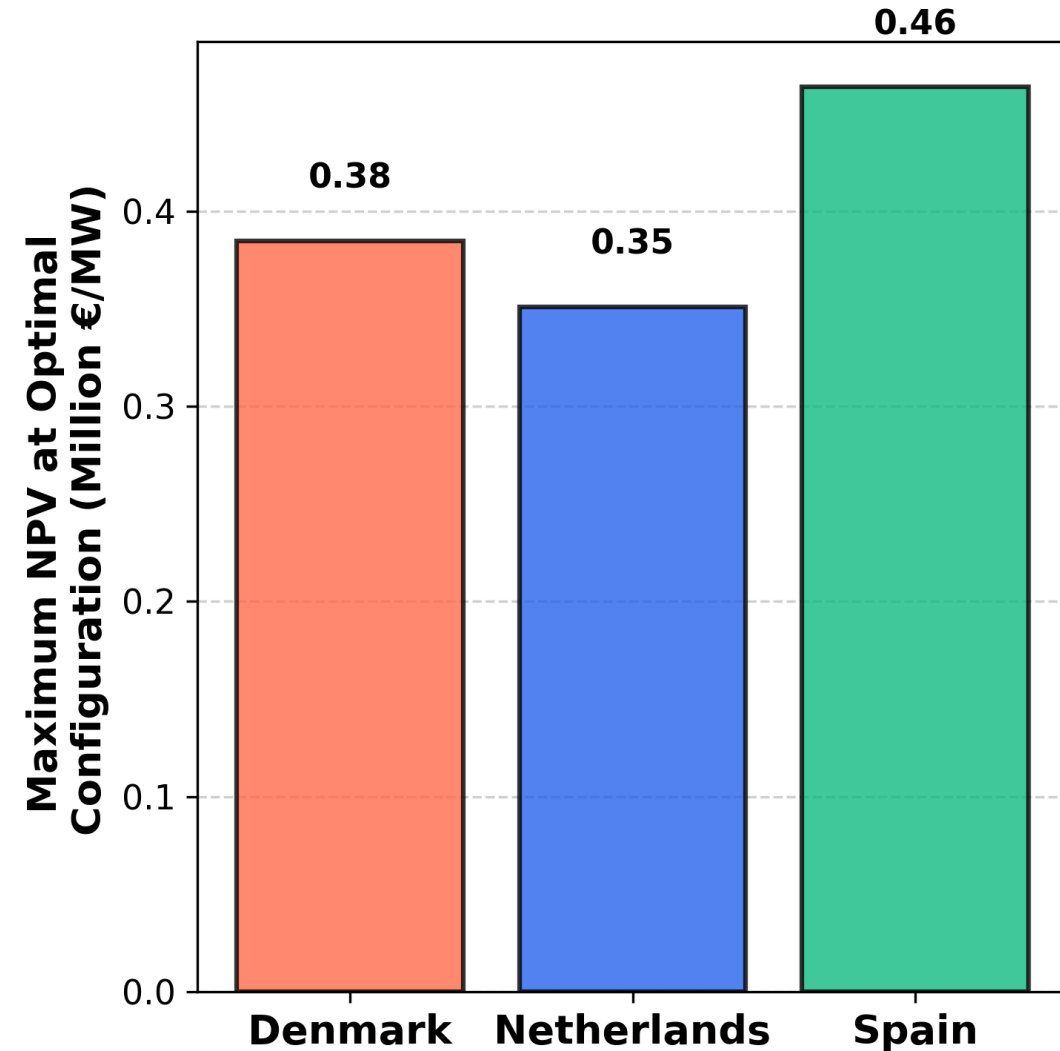
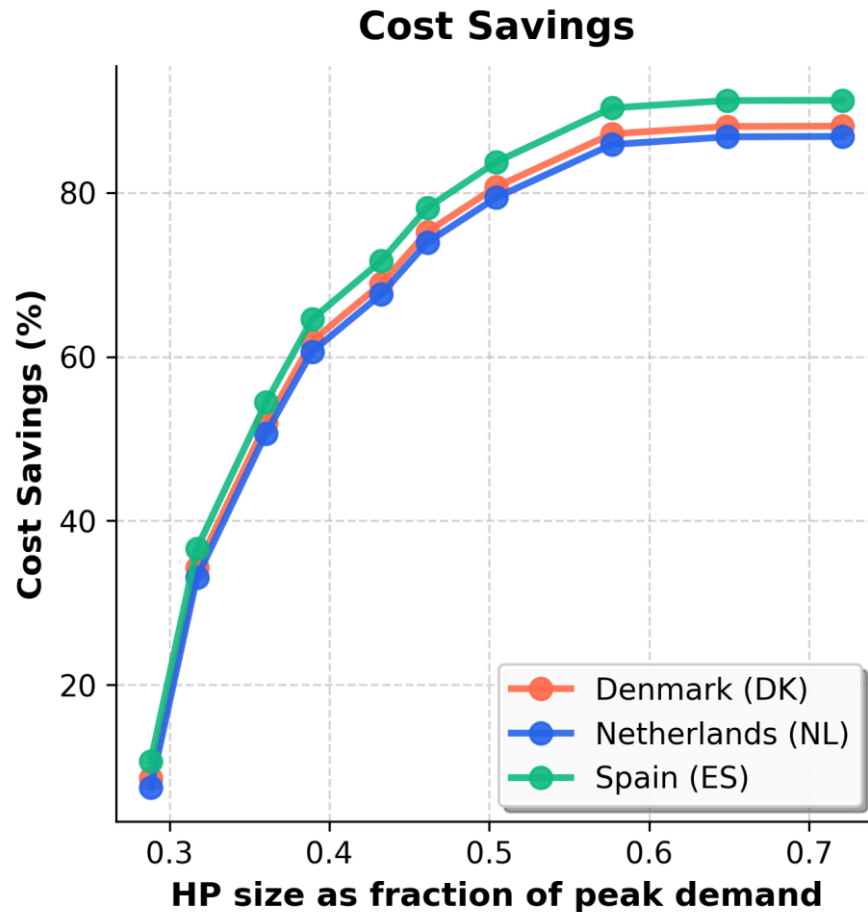
Results – price-based control of HP

HP only – no TES
considered

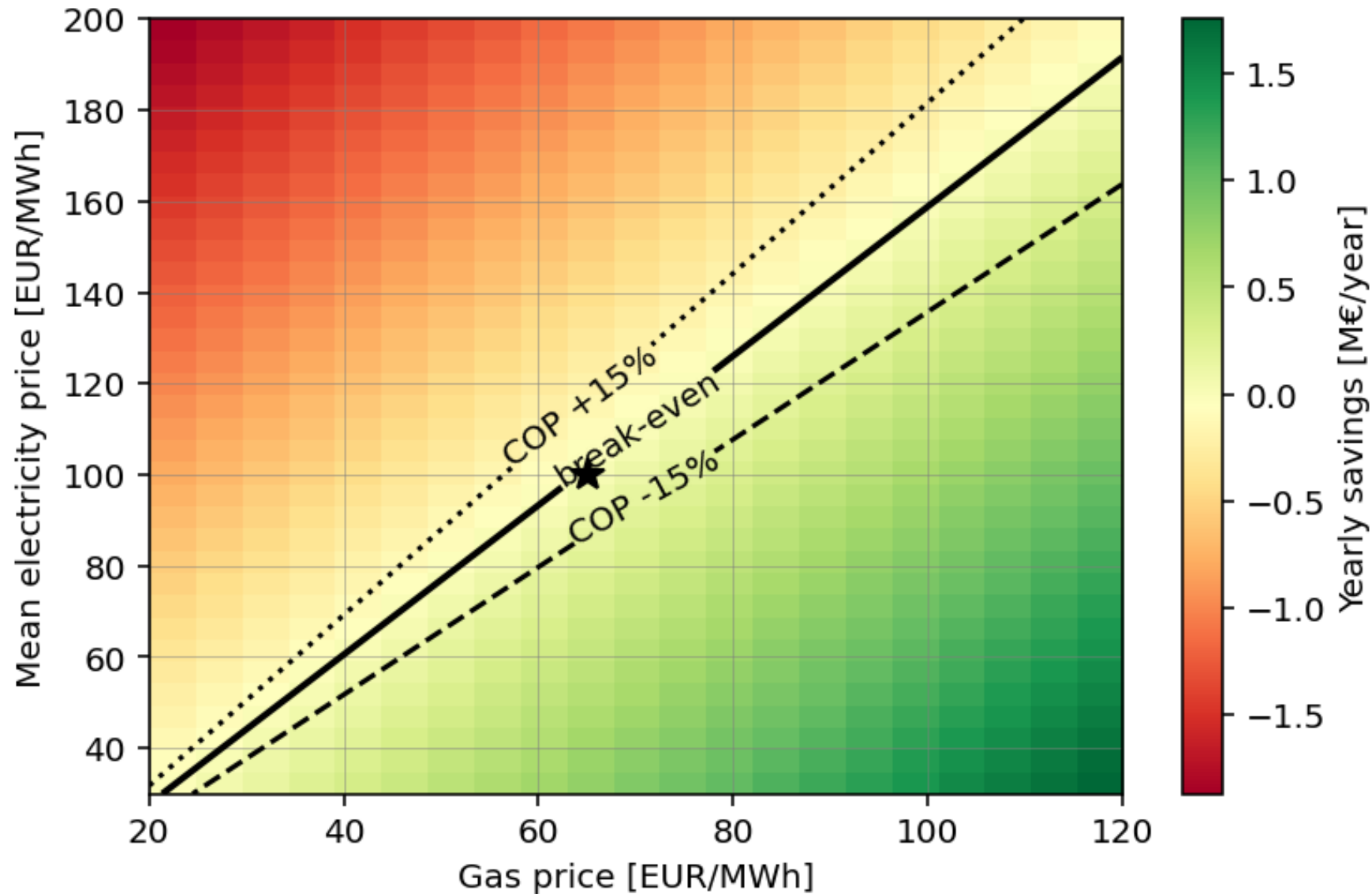


Results of the economic optimization

- Heat pump sized to deliver ~55% of the peak load
- TES can store approximately 1 h of HP capacity



Sensitivity to energy prices

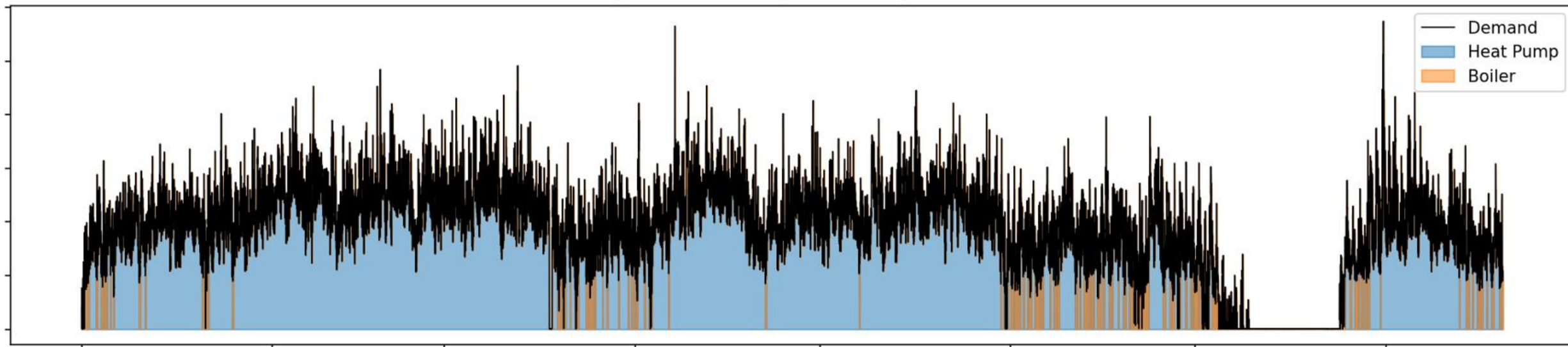


**Special case – full
electrification
with an electric
boiler and heat
pump**

Coupling heat pump and electric boiler

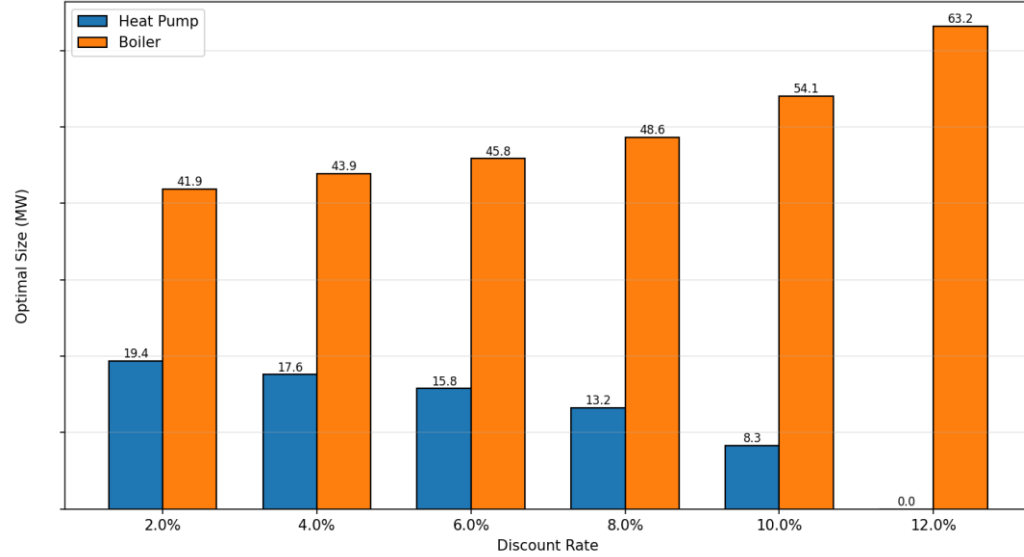


- Heat pump is always cheaper to operate when electricity price is positive so the heat pump operation becomes rules based
- Heat pump constraints
 - Min load is 40% of capacity
 - Min shutoff time is 60 min
- Maximum ramp rate is 2%/min
- Electric boiler covers demand that heat pump cannot
- Size of boiler and heat pump can be optimized using the MILP model

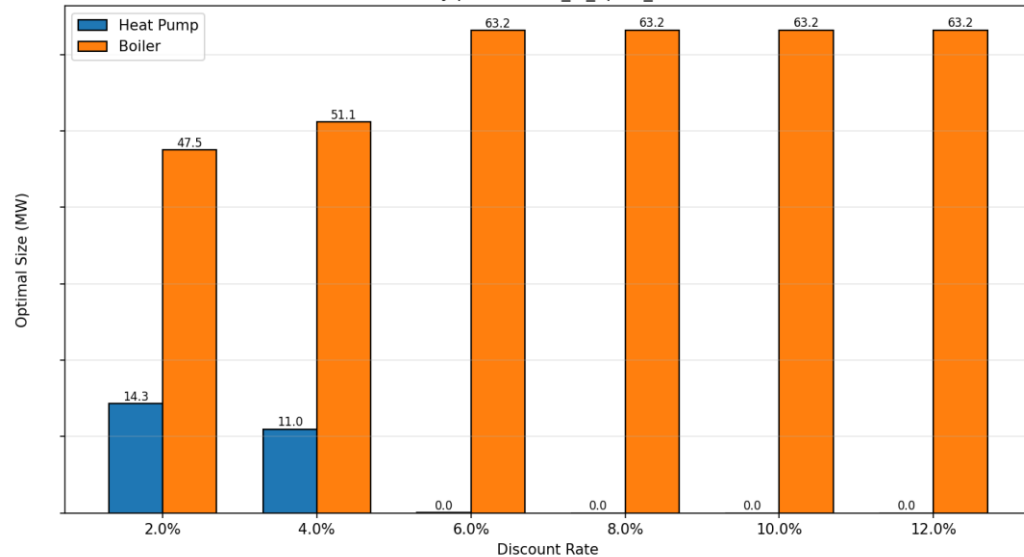


NPV optimization for different electricity markets

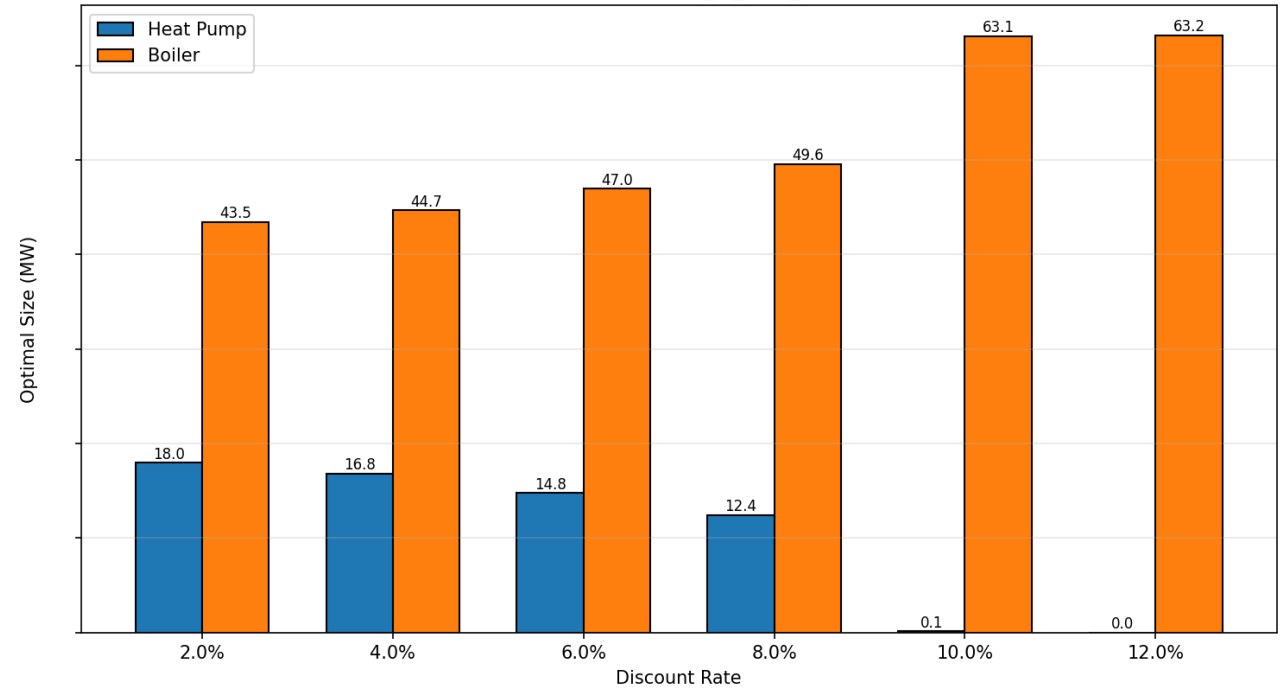
Optimal Equipment Sizes vs Discount Rate
Electricity prices: Total_EI_NL_2024.csv



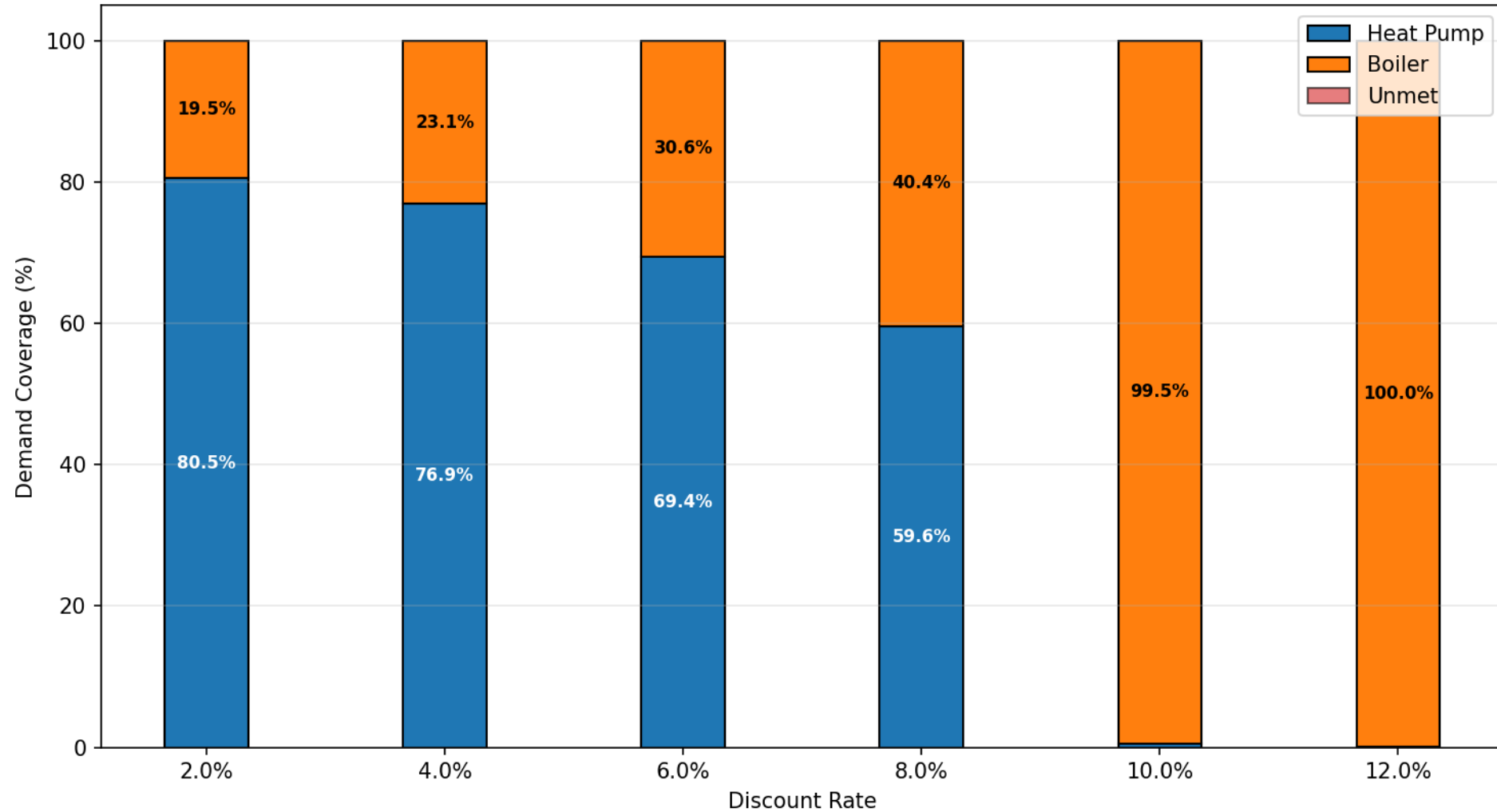
Optimal Equipment Sizes vs Discount Rate
Electricity prices: Total_EI_Spain_2024.csv



Optimal Equipment Sizes vs Discount Rate
Electricity prices: Total_EI_DK2_2024.csv



Load split for heat pump/electric boiler in Denmark



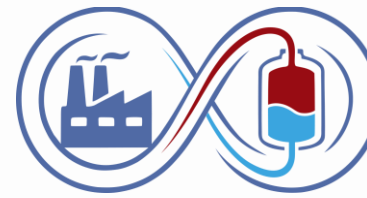
Summary and conclusions



- The CHASE project aims to demonstrate heat pumps operating at 150 °C and 250 °C coupled to latent heat thermal energy storages
- DTI has developed a technoeconomic optimization tool that can be used to evaluate the business case of implementing heat pumps, thermal energy storage and electric boilers
- In this studied case, the storage is used to cover peak demands and reduce investment in the heat pump
 - Sizing of the TES and heat pump depend on electricity pricing and demand curve
- Electricity prices, including tariffs, in Spain are more attractive for TES applications than Denmark and the Netherlands

Thermal Energy Storage for Industrial Systems - Symposium

- **Date:** 11-12 March 2027
- **Location:** Copenhagen, Denmark
- **Venue:** Langelinie Pavillonen, Langelinie 10, Copenhagen
- **Abstract Deadline:** 1 December 2026
- **Key themes:**
 - Case studies and techno-economic analyses of TES in industry.
 - Electrification of industrial heat via TES technologies.
 - System integration of TES to manage variable electricity prices and intermittent renewables.
 - High-temperature heat pumps and electric heaters in industrial applications.
 - Materials science and the development of novel materials for high-temperature TES.
 - Modelling, optimisation, and control of TES systems for industrial processes.
 - The translation of laboratory concepts to deployable, full-scale industrial solutions.



Symposium
Thermal Energy Storage
for Industrial Systems

Thank you for your attention.

keng@teknologisk.dk

This study was funded by the European Union under Clean Energy Transition Partnership (CETP) program and Innovation Fund Denmark under the project title "CHASE – Combined Heat Pump and Thermal Storage for Energy Efficient Industry

A collage of various national flags including the United Kingdom, Germany, Norway, Switzerland, Sweden, Spain, South Korea, and others.



June 2025 to May 2028



- Keep track of current and future technologies

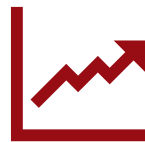
<https://heatpumpingtechnologies.org/project68/task1/>



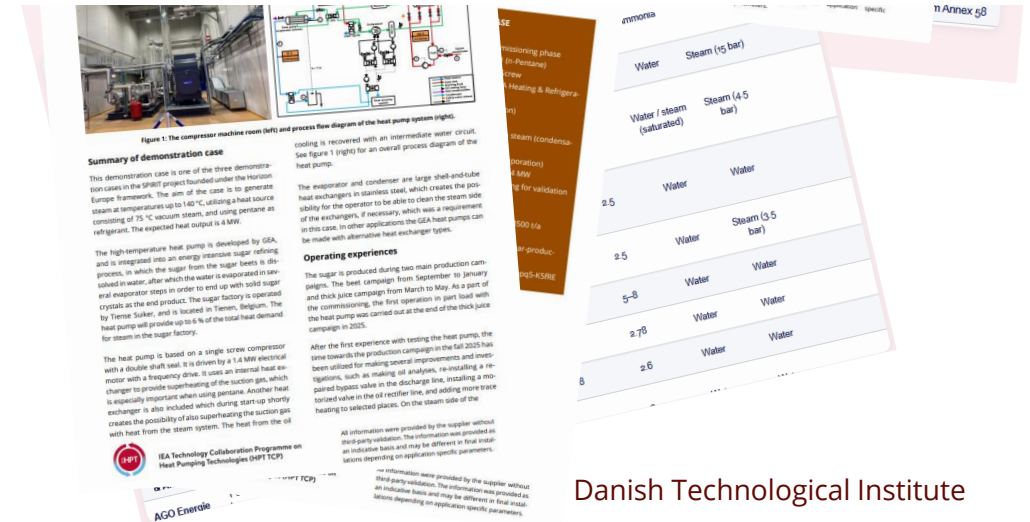
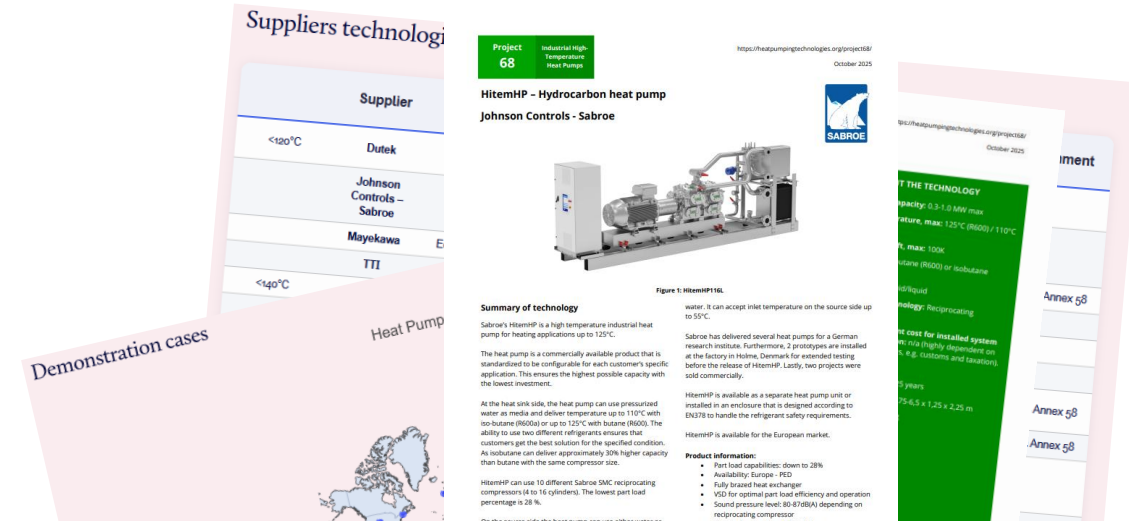
40+ Cases



55+ Technology suppliers



Newest trends



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Co-host:  **BioPhorum**

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